

Grundfos Technical Institute



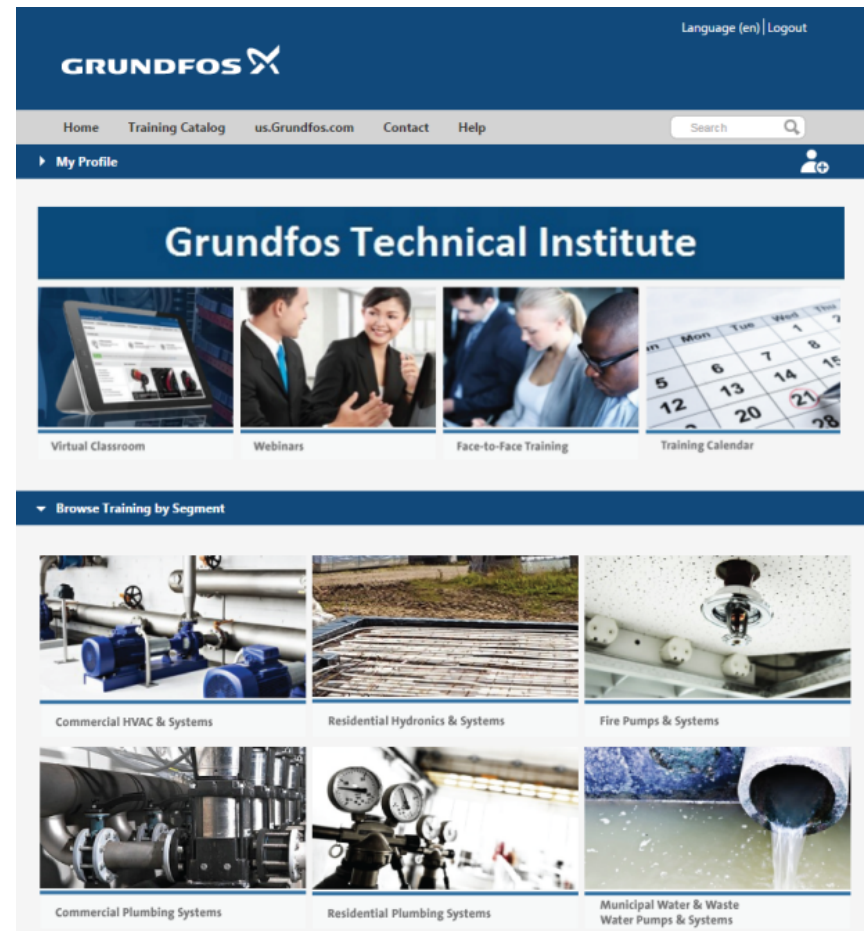
Efficient Pump Selection & Control

www.grundfos.us/training

Grundfos Technical Institute

www.grundfos.us/training

- Virtual Classroom
 - Self-Paced
 - Over 50 courses
 - Certificates of Completion
- Webinars
 - Live and Recorded
- Face-to-Face Training



Points on a Pump Performance Curve

Shut-Off Head

No flow performance, don't run here for more than a few minutes (Damage from heat buildup can occur)

Operating Point

This is where the pump is actually running, where the system curve intersects the performance curve

Duty Point

The design flow and head, this is what is required, usually based on calculations

Run Out/End of Curve

This is the maximum allowable flow rate for the pump. Flows exceeding this should be avoided (Damage can occur)

Pump Efficiency

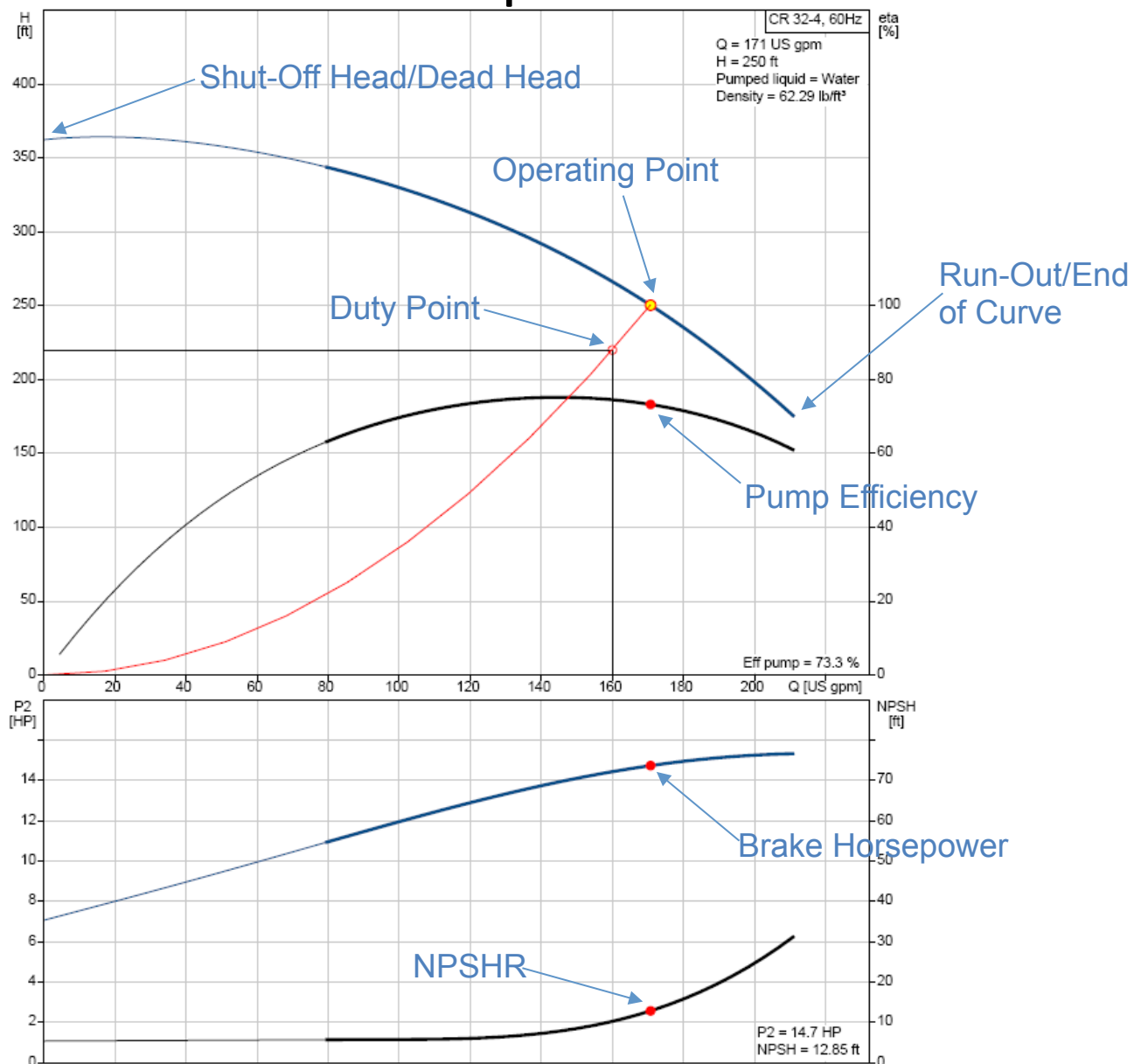
This is the pump hydraulic efficiency, does not typically include motor efficiency

Brake Horsepower

This is the horsepower required by the pump. Any point on this curve should be lower than the motor nameplate horsepower

NPSH

Net Positive Suction Head, the actual suction head of the system must be higher than this value. Very important in boiler feed systems and systems with flooded suction. Not so important for cold water from a pressurized source or hydronic heating/cool systems



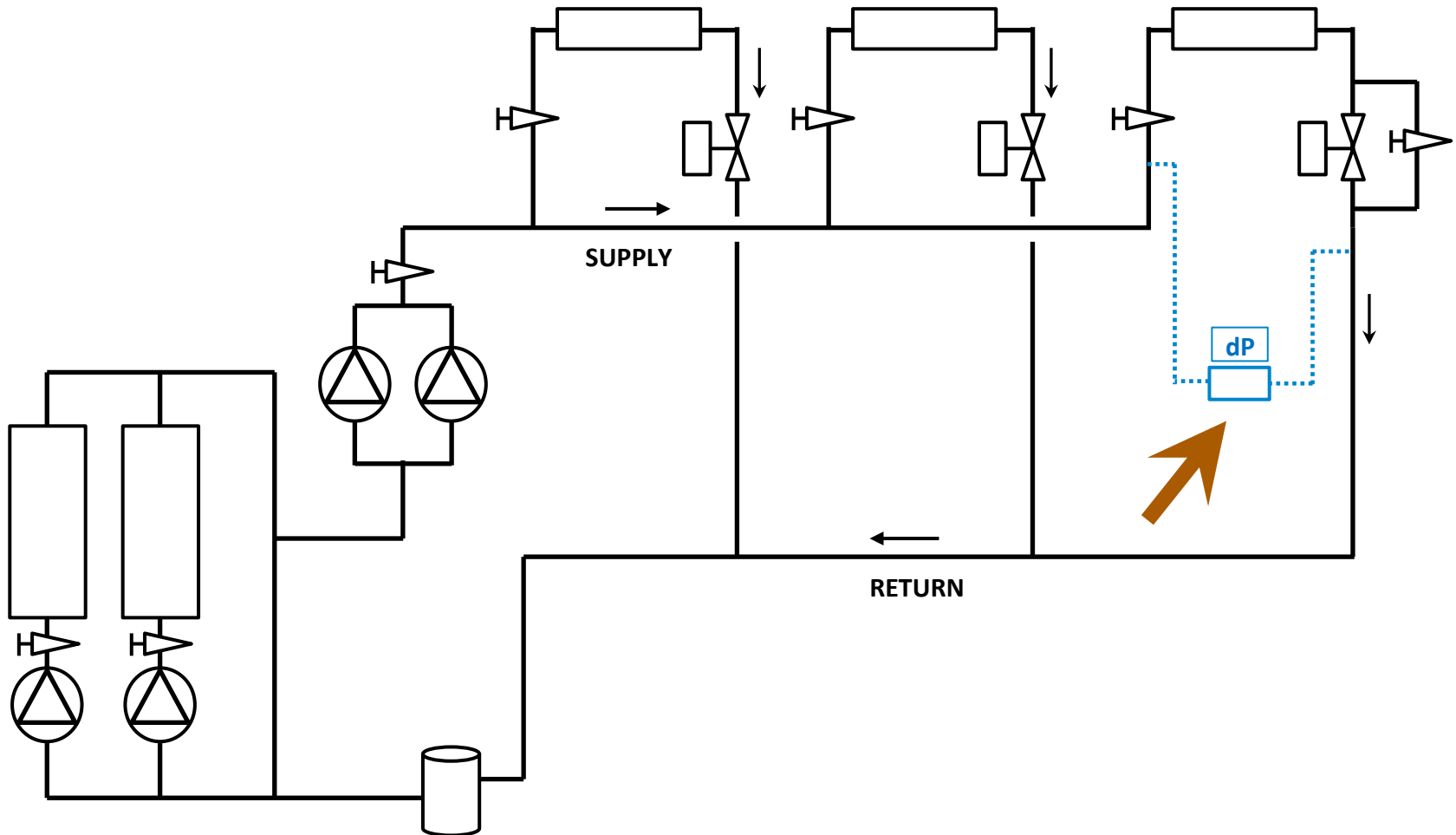
Two common variable flow pump applications

HVAC Circulation – Hot and/or Chilled Water

Water Supply – Pressure Boosting

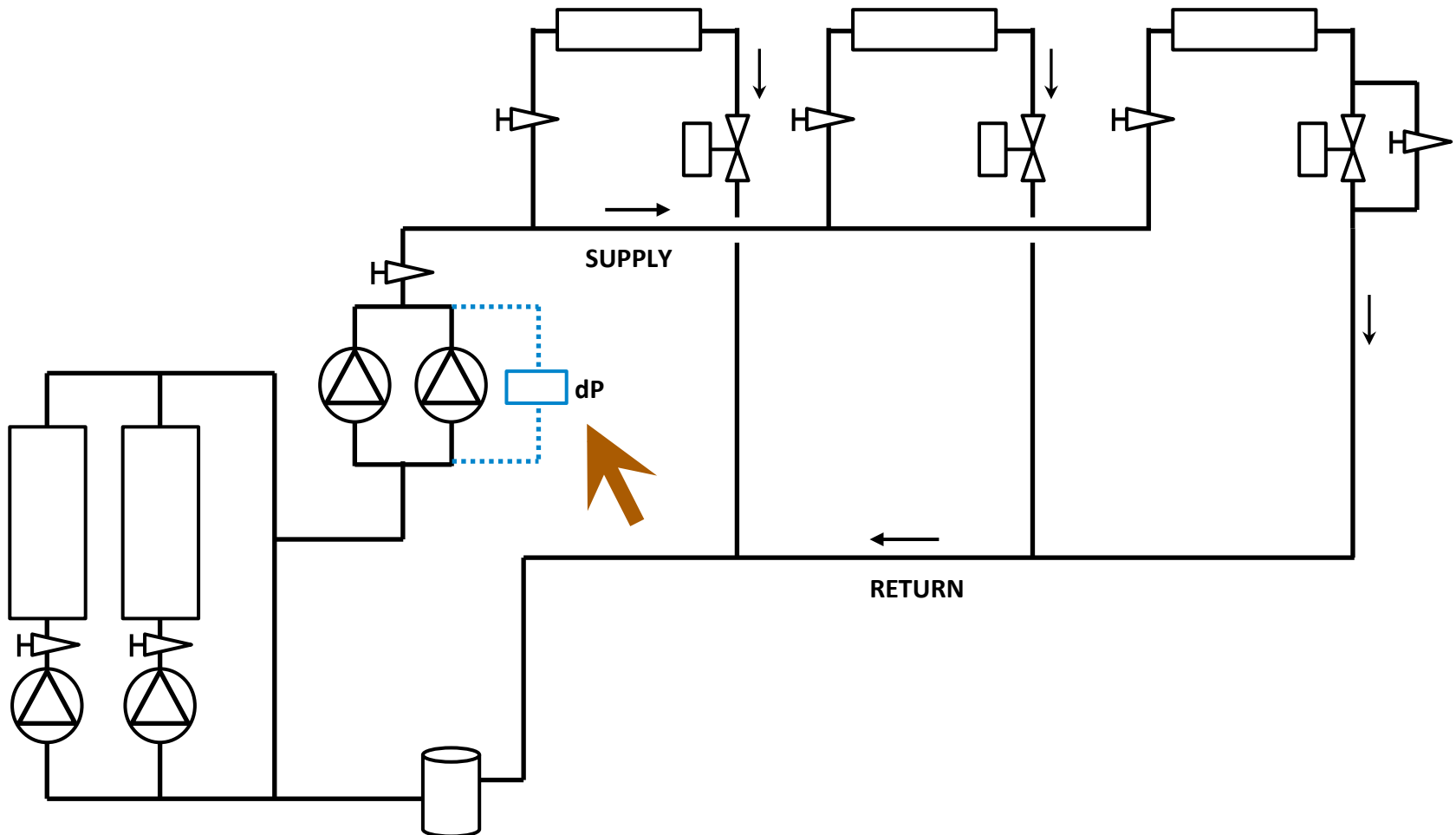
HVAC Circulation

Differential Pressure measured remotely

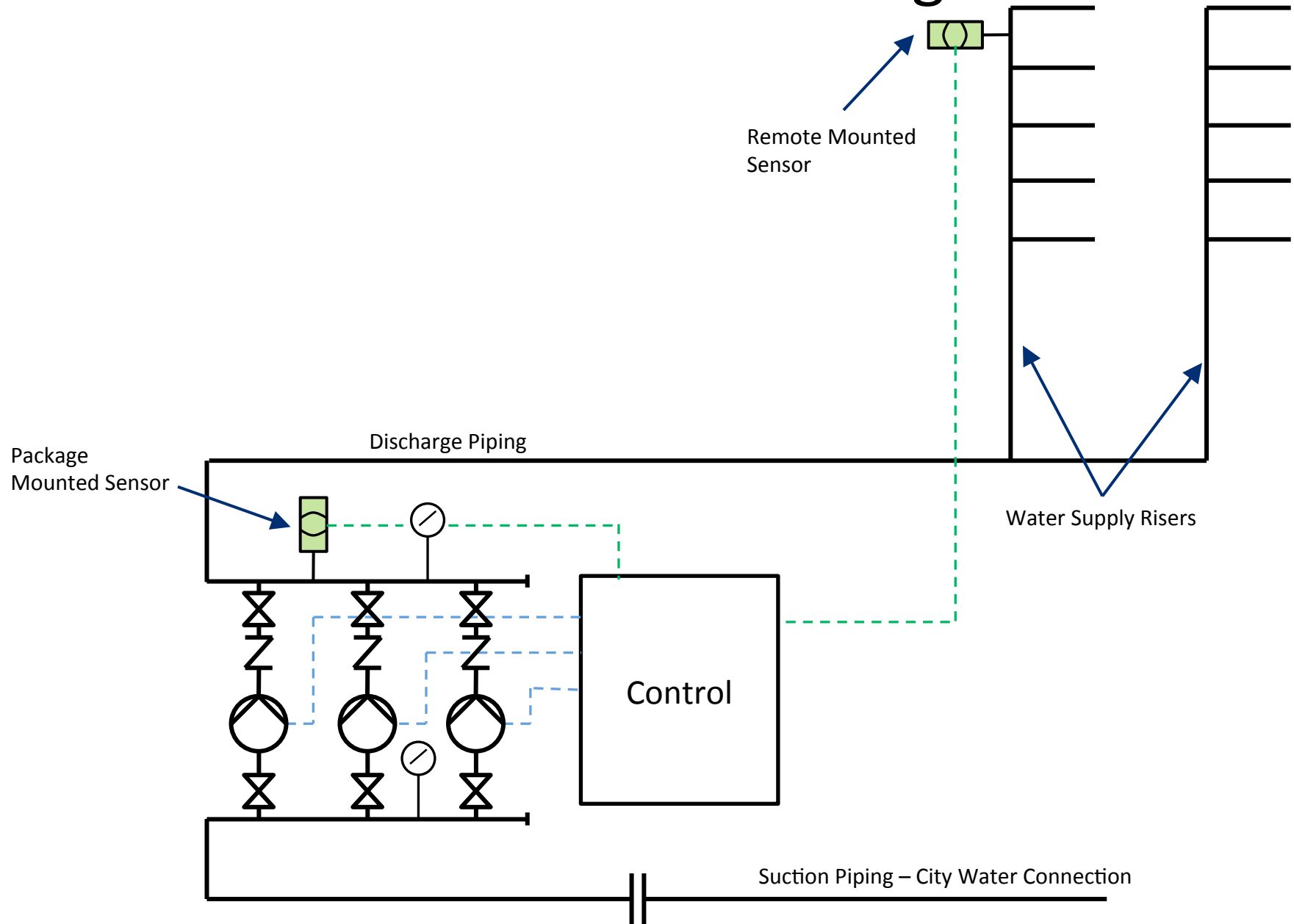


HVAC Circulation

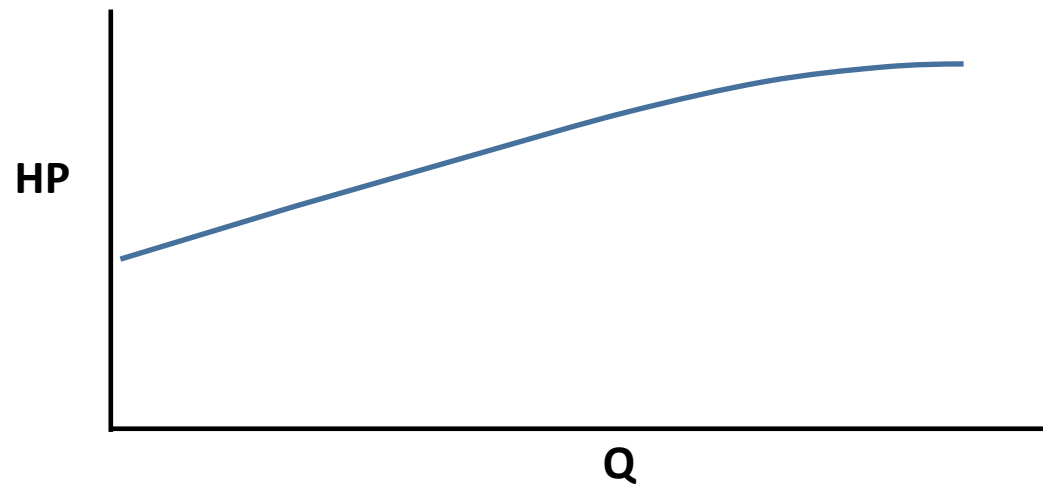
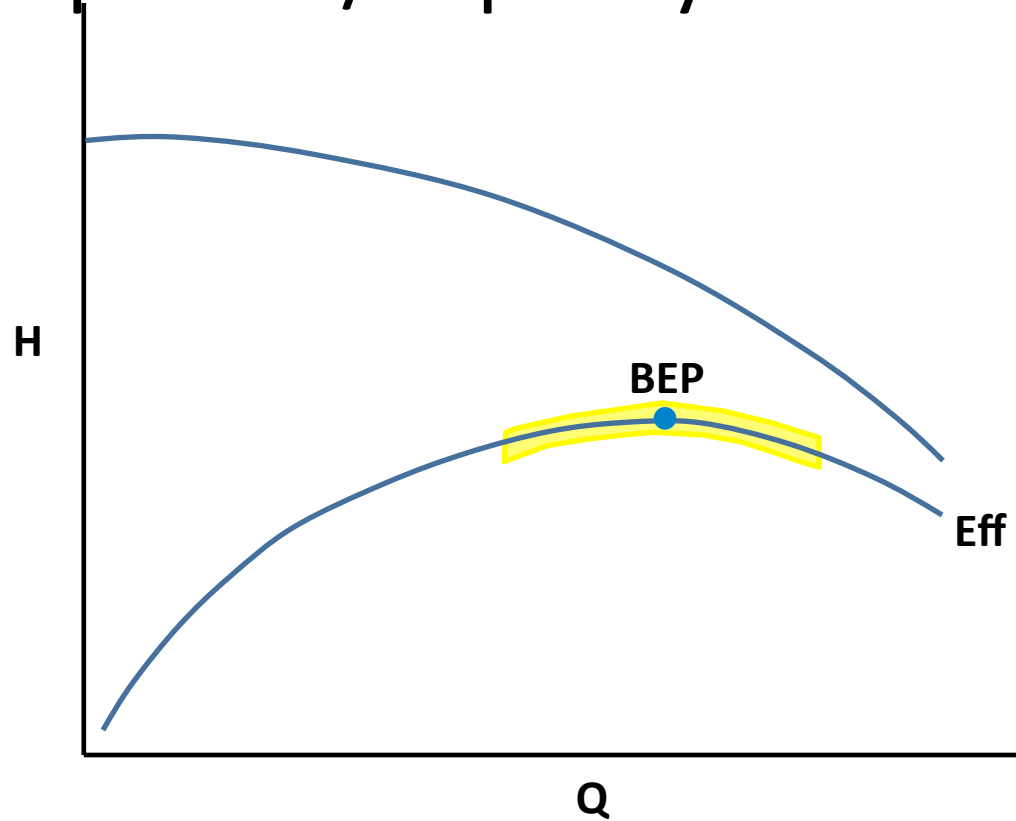
Differential Pressure measured across pumps



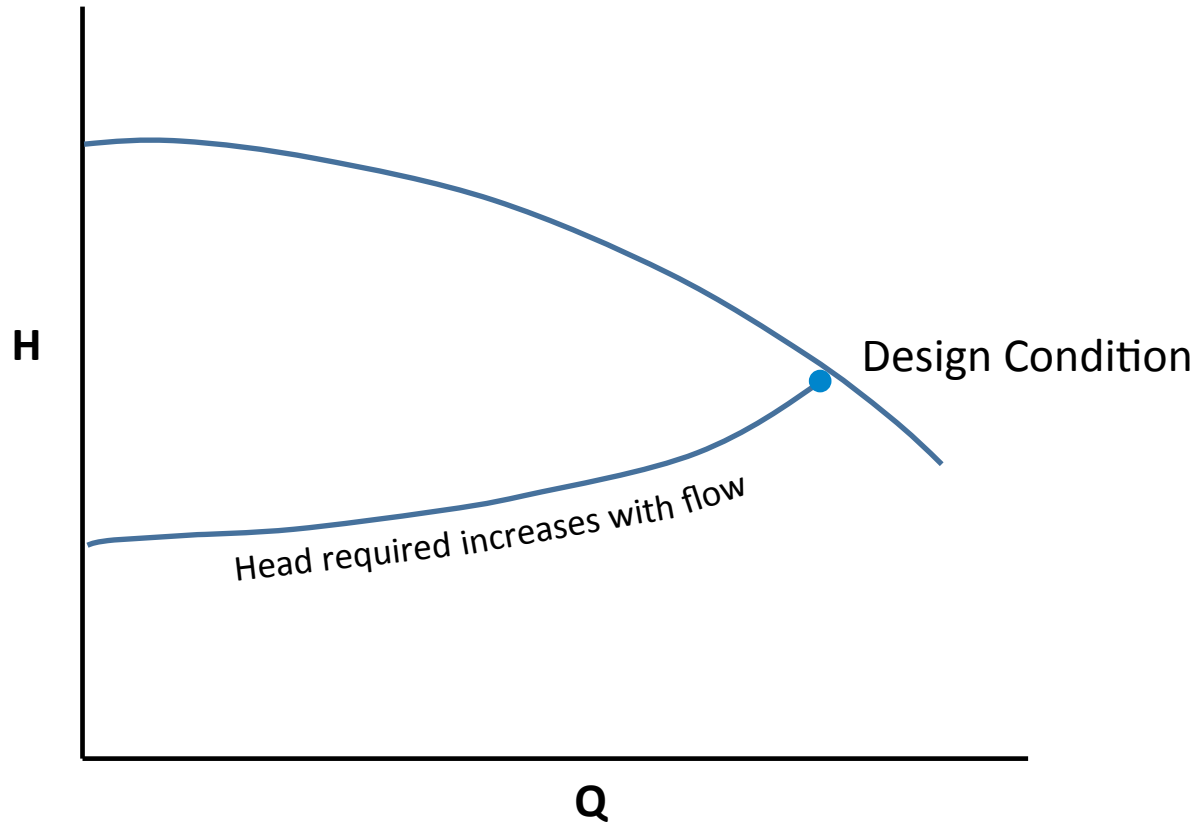
Pressure Boosting



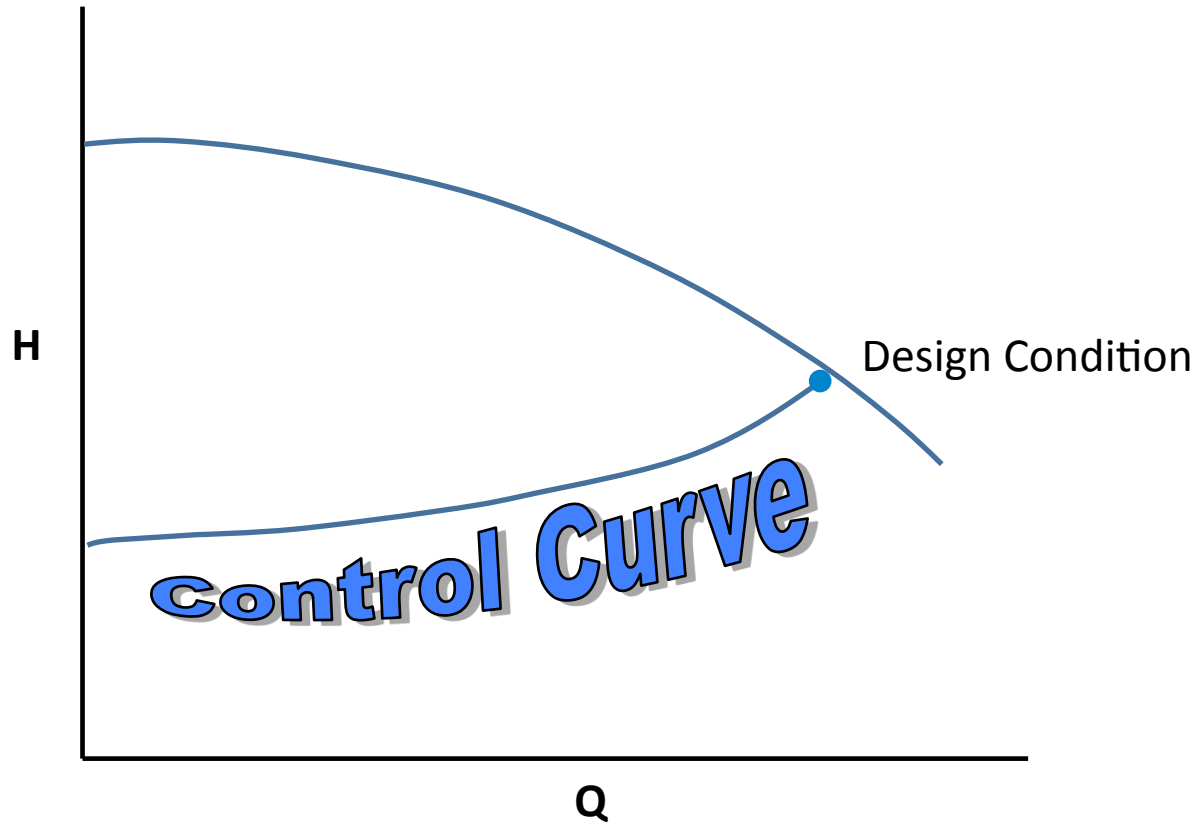
Pump Head/Capacity Curve



Pump Head/Capacity Curve



Pump Head/Capacity Curve



The Affinity Laws

for centrifugal pumps

**Flow varies linearly
with pump speed**

>

$$\frac{\text{GPM}_1}{\text{GPM}_2} = \frac{\text{RPM}_1}{\text{RPM}_2}$$

>

$$\text{GPM}_2 = \text{GPM}_1 \left(\frac{\text{RPM}_2}{\text{RPM}_1} \right)$$

**Head varies with the
square of the pump
speed**

>

$$\frac{\text{TDH}_1}{\text{TDH}_2} = \left(\frac{\text{RPM}_1}{\text{RPM}_2} \right)^2$$

>

$$\text{TDH}_2 = \text{TDH}_1 \left(\frac{\text{RPM}_2}{\text{RPM}_1} \right)^2$$

**Brake Horsepower
varies with the cube
of the pump speed**

>

$$\frac{\text{BHP}_1}{\text{BHP}_2} = \left(\frac{\text{RPM}_1}{\text{RPM}_2} \right)^3$$

>

$$\text{BHP}_2 = \text{BHP}_1 \left(\frac{\text{RPM}_2}{\text{RPM}_1} \right)^3$$

When TDH_1 , RPM_1 and TDH_2 are known:

$$\text{RPM}_2 = \text{RPM}_1 \sqrt{\frac{\text{TDH}_2}{\text{TDH}_1}}$$

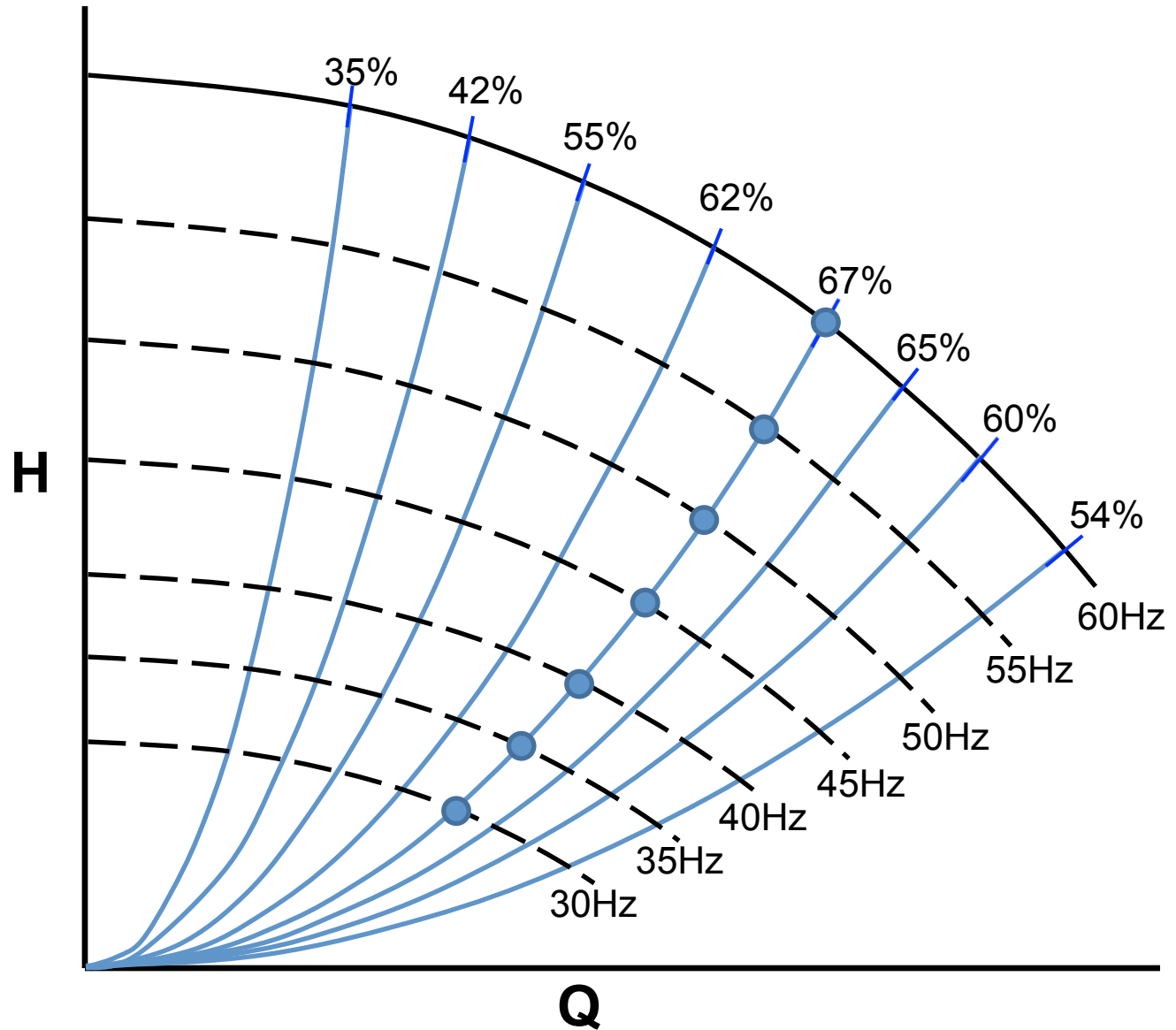
1 = Original condition (full speed)
2 = New condition (reduced speed)

What about efficiency?

Curves of constant efficiency with speed reductions

Remember....the affinity laws assume constant pump efficiency.

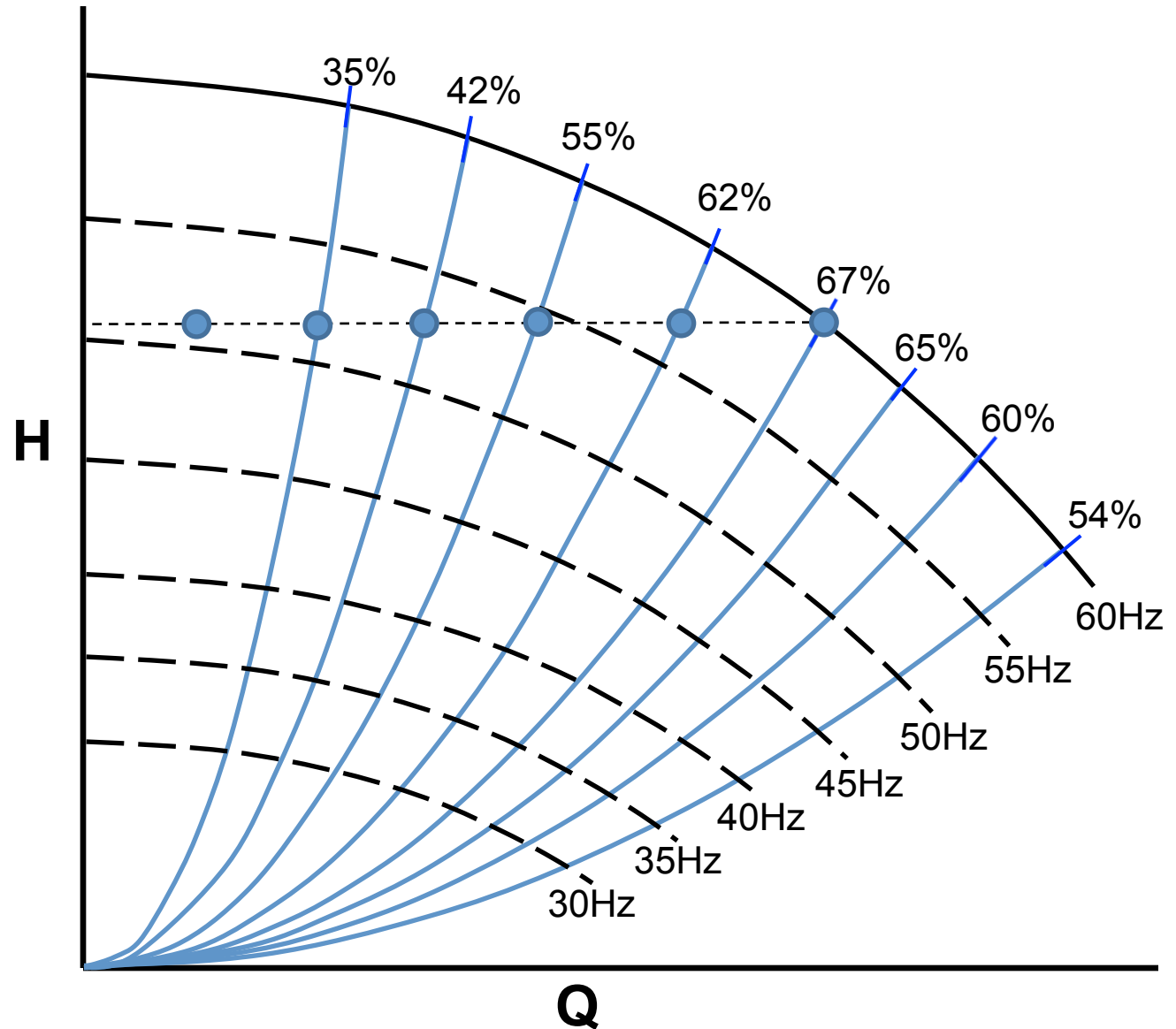
The pump can only run continuously at its **Best Efficiency Point** along a system or control curve that follows a curve of constant efficiency



Curves of constant efficiency with speed reductions

Constant Pressure:

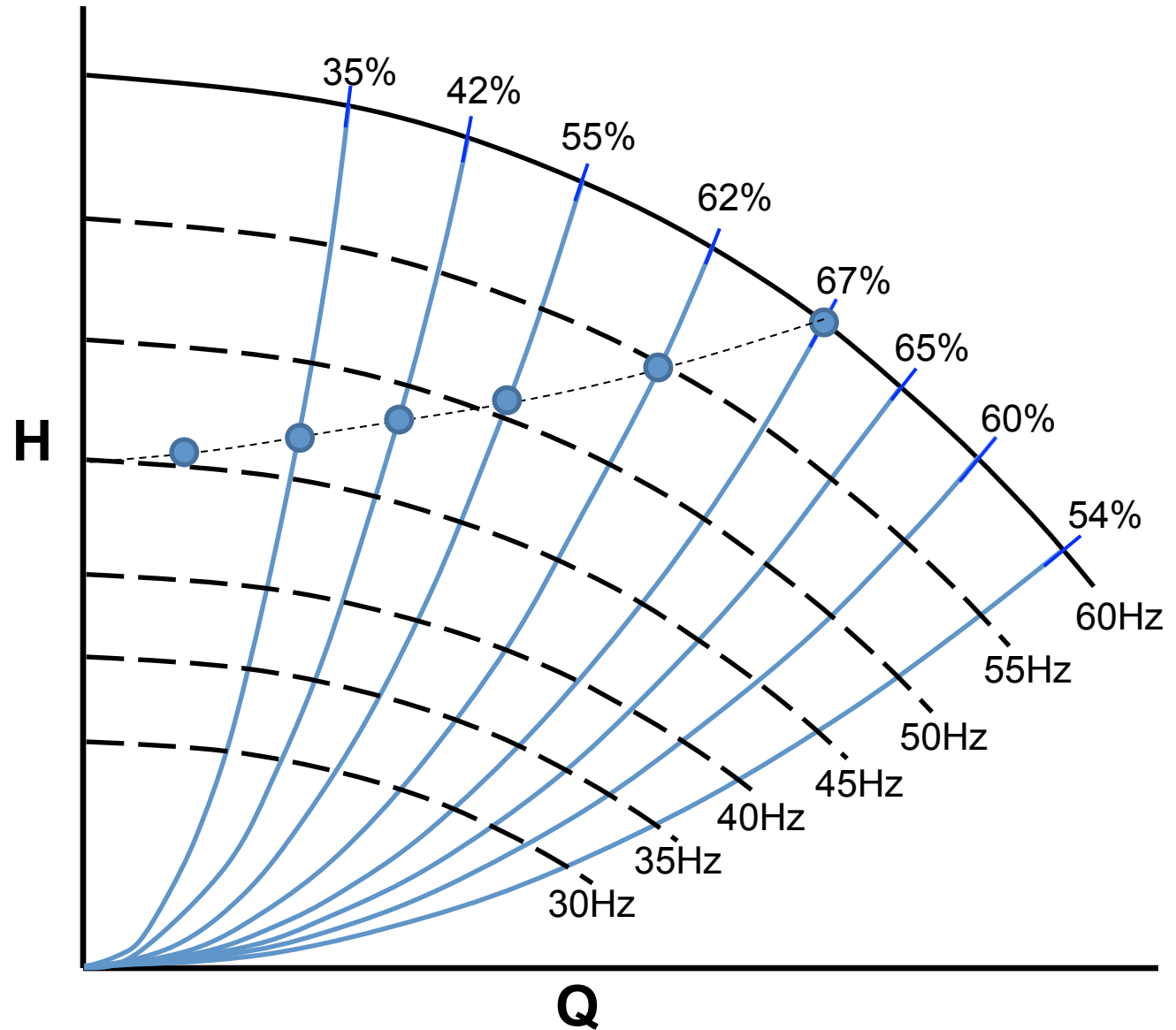
As flow reduces so
does pump efficiency!



Curves of constant efficiency with speed reductions

Similarly with HVAC
Circulation

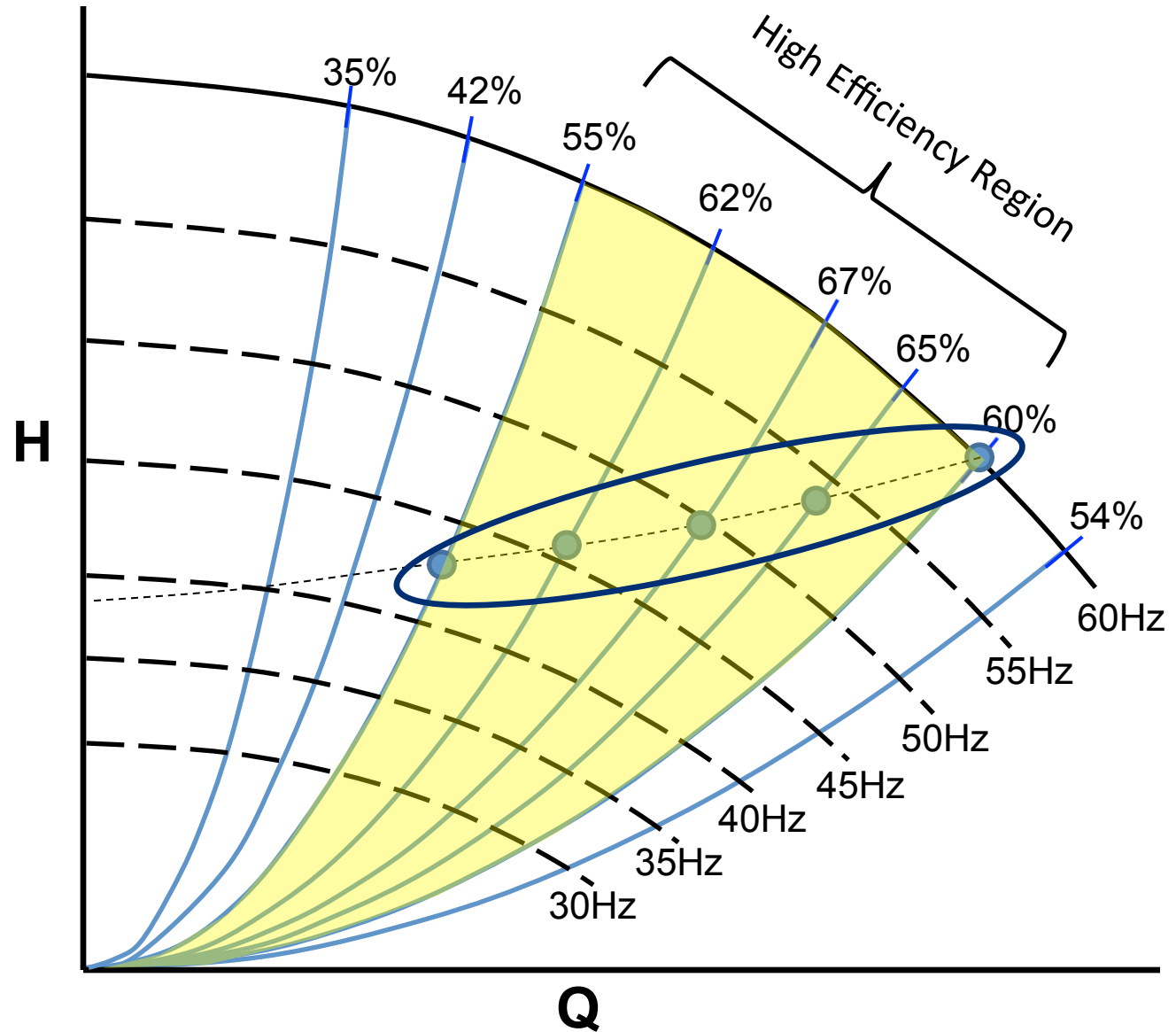
Efficiency also reduces
with reducing flow



Curves of constant efficiency with speed reductions

When selecting pumps for variable flow

Select pumps based on a design flow that is to the **RIGHT** of the pumps best efficiency point.



Pump Selection Example

Design Flow: 1000 gpm

Design Head: 75 feet

Pump Selection Example

Design Flow: 1000 gpm

Design Head: 75 feet

Selection Tool Results:

Pump	Pump Speed [rpm]	Pump Efficiency [%]	NPSHr	Max. Power [bhp]	% Max. Diameter	Size [Suc/Dis]
Option 1	1750	83.16	9.25	26.7	97.60	6 x 5
Option 2	1750	82.94	8.39	25.5	81.24	6 x 5
Option 3	1750	80.03	12.7	24.7	81.24	5 x 4
Option 4	1750	78.09	27.2	24.2	92.69	5 x 4
Option 5	1750	83.71	10.1	24.8	89.80	6 x 5

Pump Selection Example

Design Flow: 1000 gpm

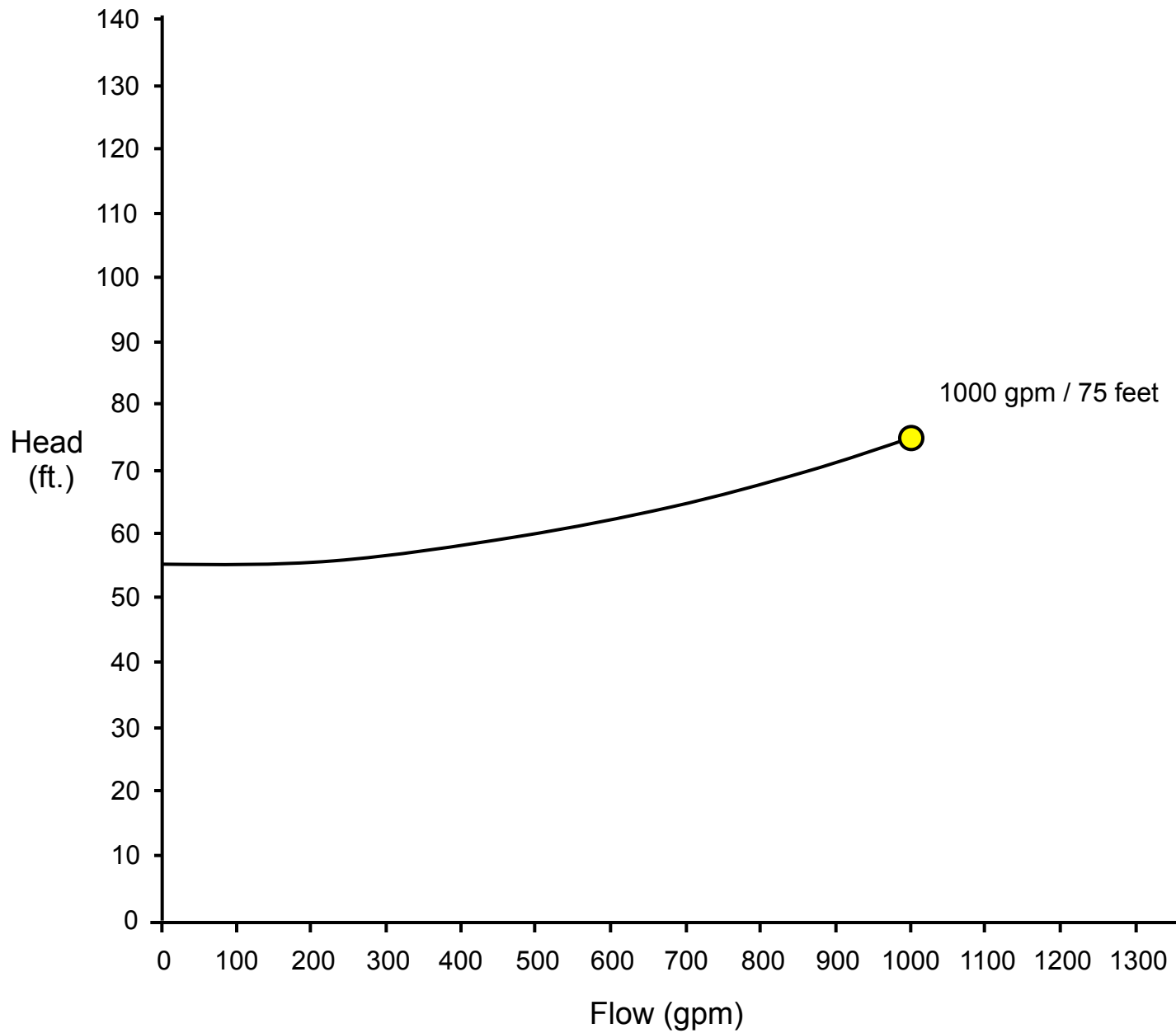
Design Head: 75 feet

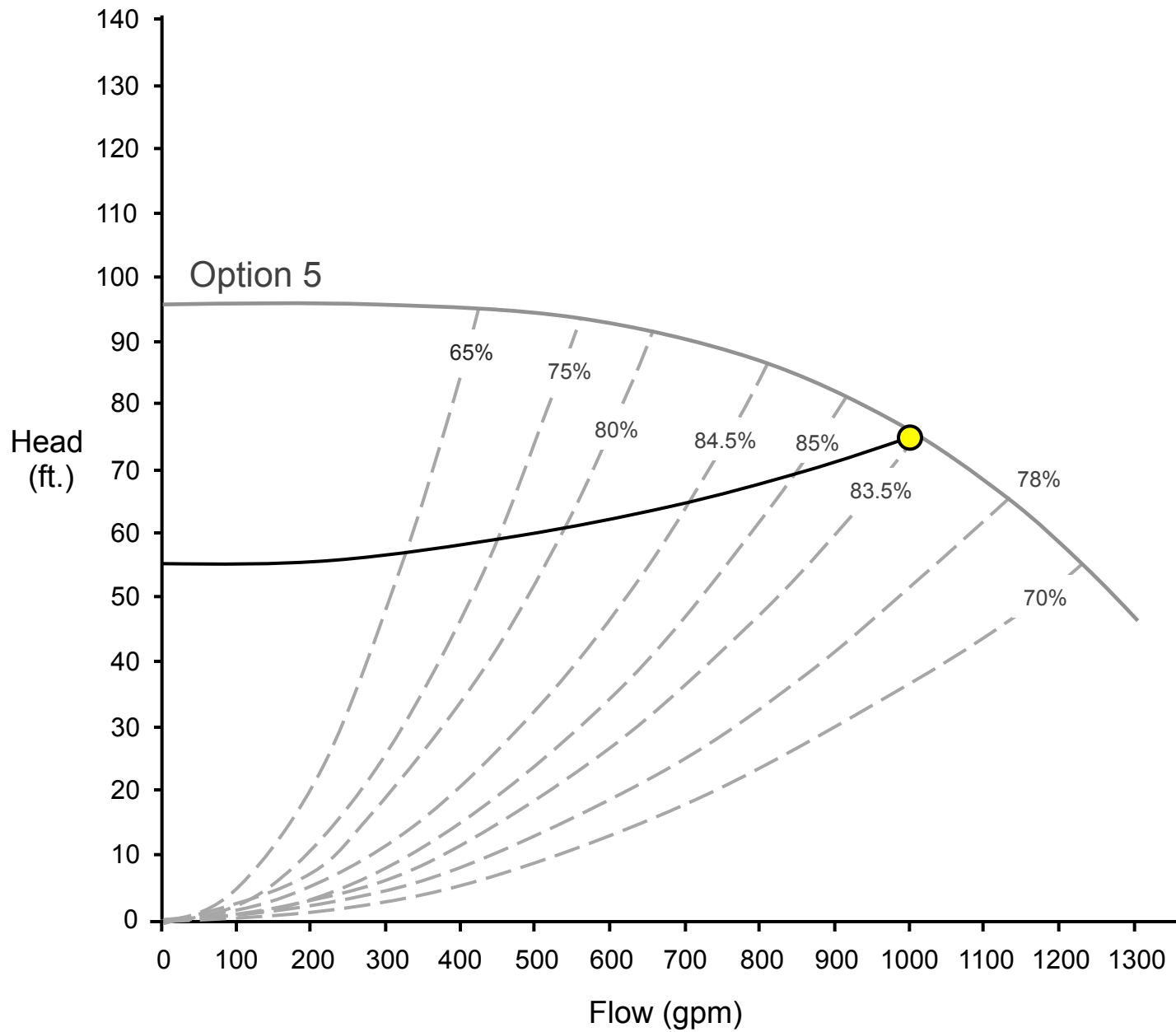
Selection Tool Results:

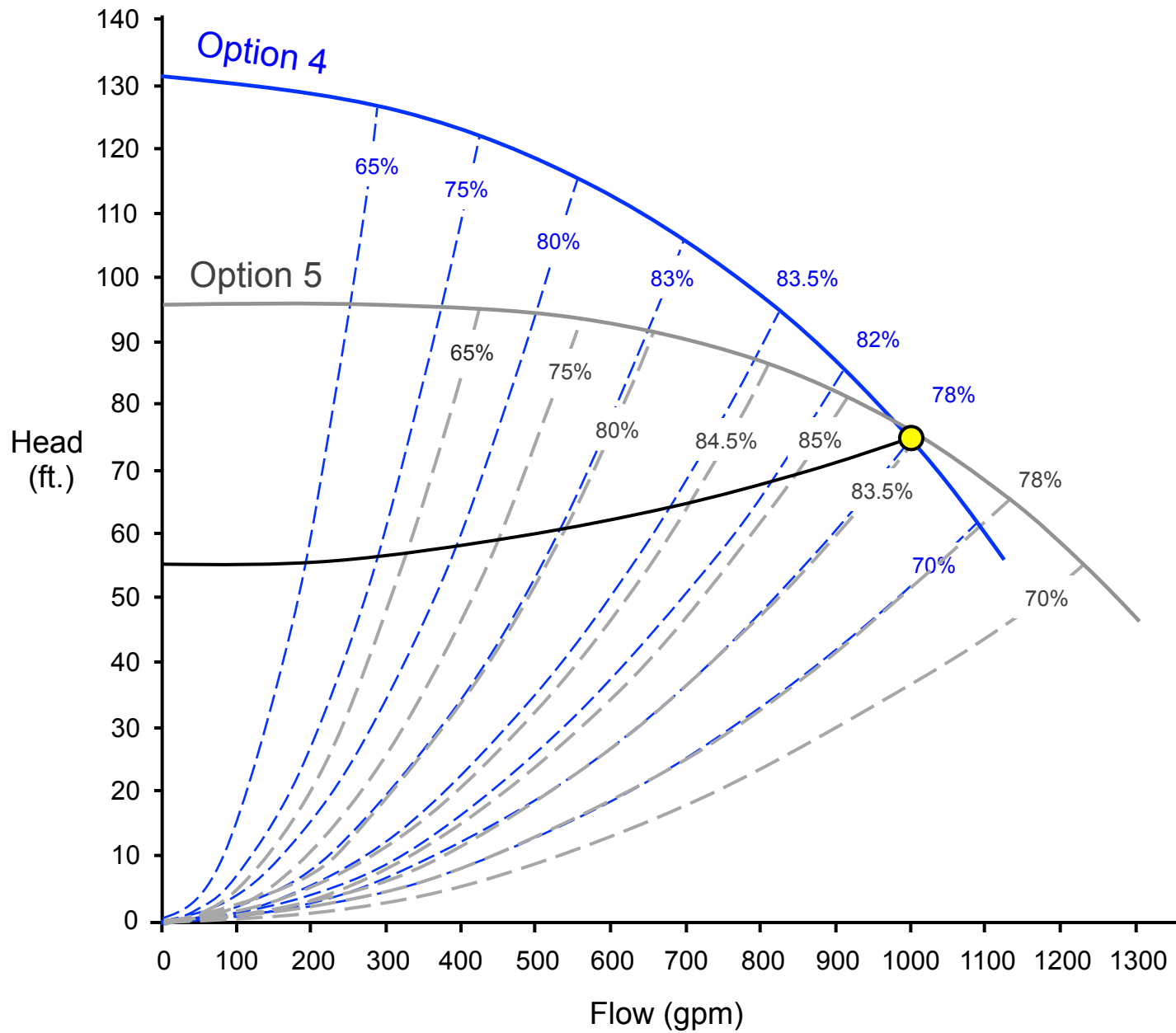
Pump	Pump Speed [rpm]	Pump Efficiency [%]	NPSHr	Max. Power [bhp]	% Max. Diameter	Size [Suc/Dis]
Option 1	1750	83.16	9.25	26.7	97.60	6 x 5
Option 2	1750	82.94	8.39	25.5	81.24	6 x 5
Option 3	1750	80.03	12.7	24.7	81.24	5 x 4
Option 4	1750	78.09	27.2	24.2	92.69	5 x 4
Option 5	1750	83.71	10.1	24.8	89.80	6 x 5

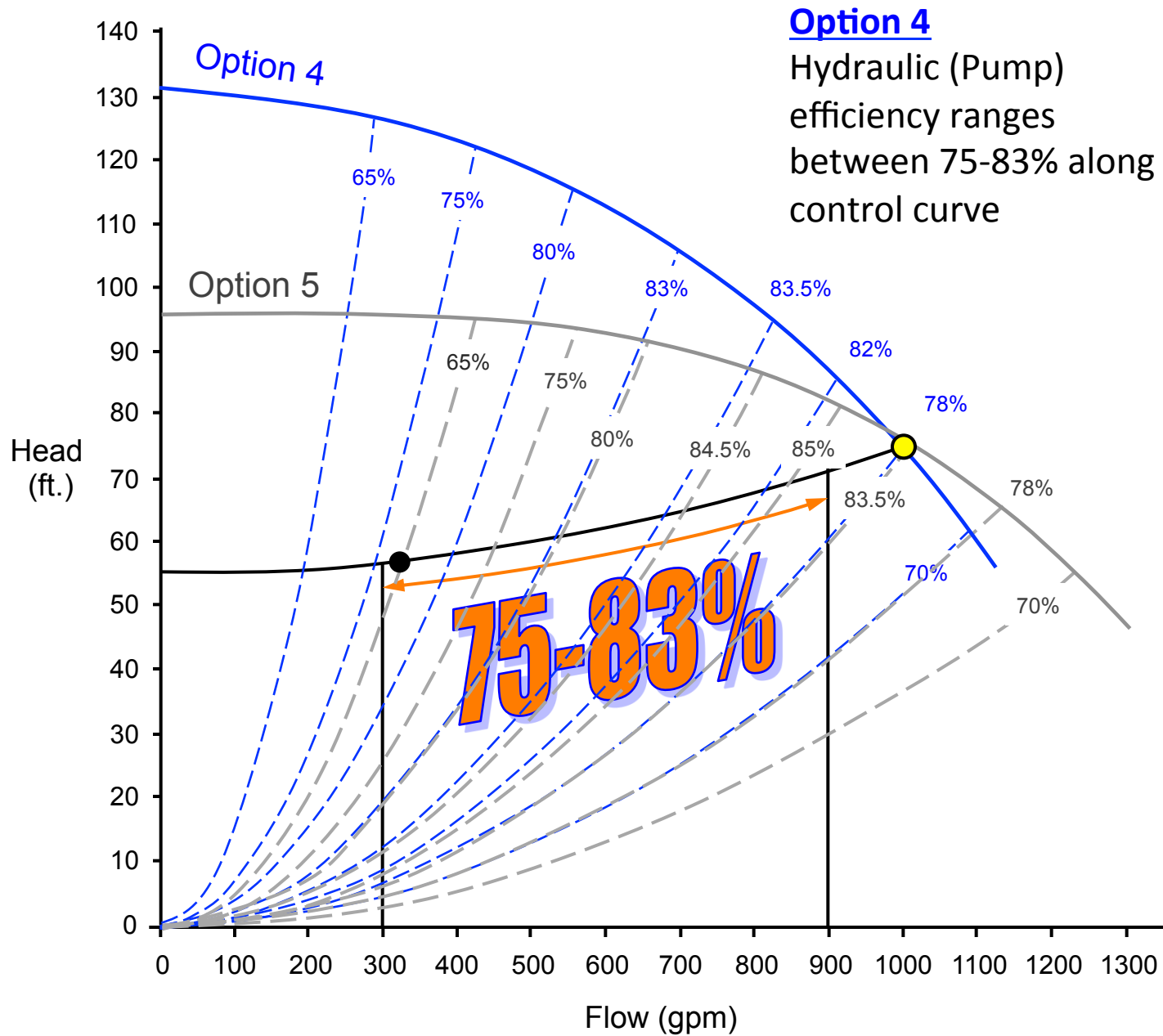
Option 5 = Highest efficiency, but is it the best choice for **variable** flow?

You must look at the pump curves as well as the control curve!









Enter Flow Profile - 5 Duty Points

Flow (GPM)	Required TDH, feet	Hours per Day	Hours per Yr
300.0	57	5.0	1,250
500.0	60	4.0	1,000
600.0	62	3.0	750
700.0	65	2.0	500
900.0	71	1.0	250
		15	3,750

Enter Flow Profile - 5 Duty Points

Flow (GPM)	Required TDH, feet	Hours per Day	Hours per Yr
300.0	57	5.0	1,250
500.0	60	4.0	1,000
600.0	62	3.0	750
700.0	65	2.0	500
900.0	71	1.0	250
		15	3,750

Brake Horsepower

Flow	Option 1	Option 2	Option 3	Option 4	Option 5
300	7.3	9.5	6.9	5.7	6.9
500	10.1	12.1	9.8	9.2	9.7
600	11.8	13.6	11.7	11.3	11.4
700	13.9	15.5	14.1	13.7	13.5
900	19.4	19.9	19.9	20.2	19.1

Energy [kWh]

Flow	Option 1	Option 2	Option 3	Option 4	Option 5
300	7994.2	9978.5	7288.8	6322.3	7310.3
500	8473.2	10164.2	8357.4	7802.3	8212.9
600	7472.7	8611.7	7480.1	7183.3	7267.5
700	5860.5	6464.0	5929.2	5793.9	5715.7
900	4046.4	4165.6	4210.4	4274.1	4031.9
	33847.1	39384.0	33265.9	31375.8	32538.4

Efficiency

Flow	Option 1	Option 2	Option 3	Option 4	Option 5
300	59.1	45.3	62.8	75.8	62.6
500	75.4	62.6	77.1	82.6	78.5
600	79.6	69.0	80.2	83.6	82.4
700	82.1	74.2	81.6	83.4	84.5
900	83.4	81.1	81.1	80.3	84.7

Pump	Pump Speed [rpm]	Pump Efficiency [%]	NPSHr	Max. Power [bhp]	% Max. Diameter	Size [Suc/Dis]
Option 1	1750	83.16	9.25	26.7	97.60	6 x 5
Option 2	1750	82.94	8.39	25.5	81.24	6 x 5
Option 3	1750	80.03	12.7	24.7	81.24	5 x 4
Option 4	1750	78.09	27.2	24.2	92.69	5 x 4
Option 5	1750	83.71	10.1	24.8	89.80	6 x 5

Option 4 has the lowest energy consumption, yet the lowest efficiency at the design flow. How many hours do you really run at design flow, if ever.....

Multiple Pump Operation - Parallel

Example:

Basic Requirements

Design Flow: 350 gpm

Design TDH: 90 feet

Question:

Do we just select a 350 gpm pump with a head capacity of 90 feet and be done with it?

Load Profile

Edit Load Profile

Load profile

User profile

Yearly operation time

250

days

Duty point

Flow

Q

Hours

1

100

%

350

US GPM

267

h/a

2

75

%

263

US GPM

667

h/a

3

50

%

175

US GPM

1466

h/a

4

25

%

87.5

US GPM

3600

h/a

Q
[US GPM]

350.0

263.0

175.0

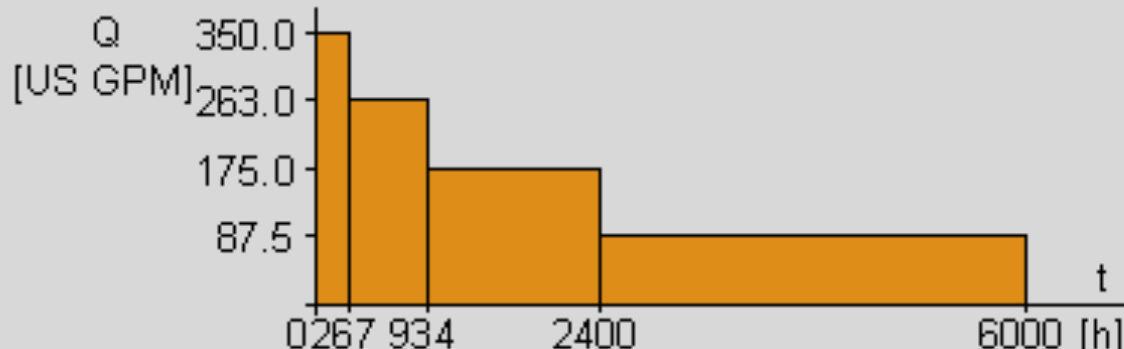
87.5

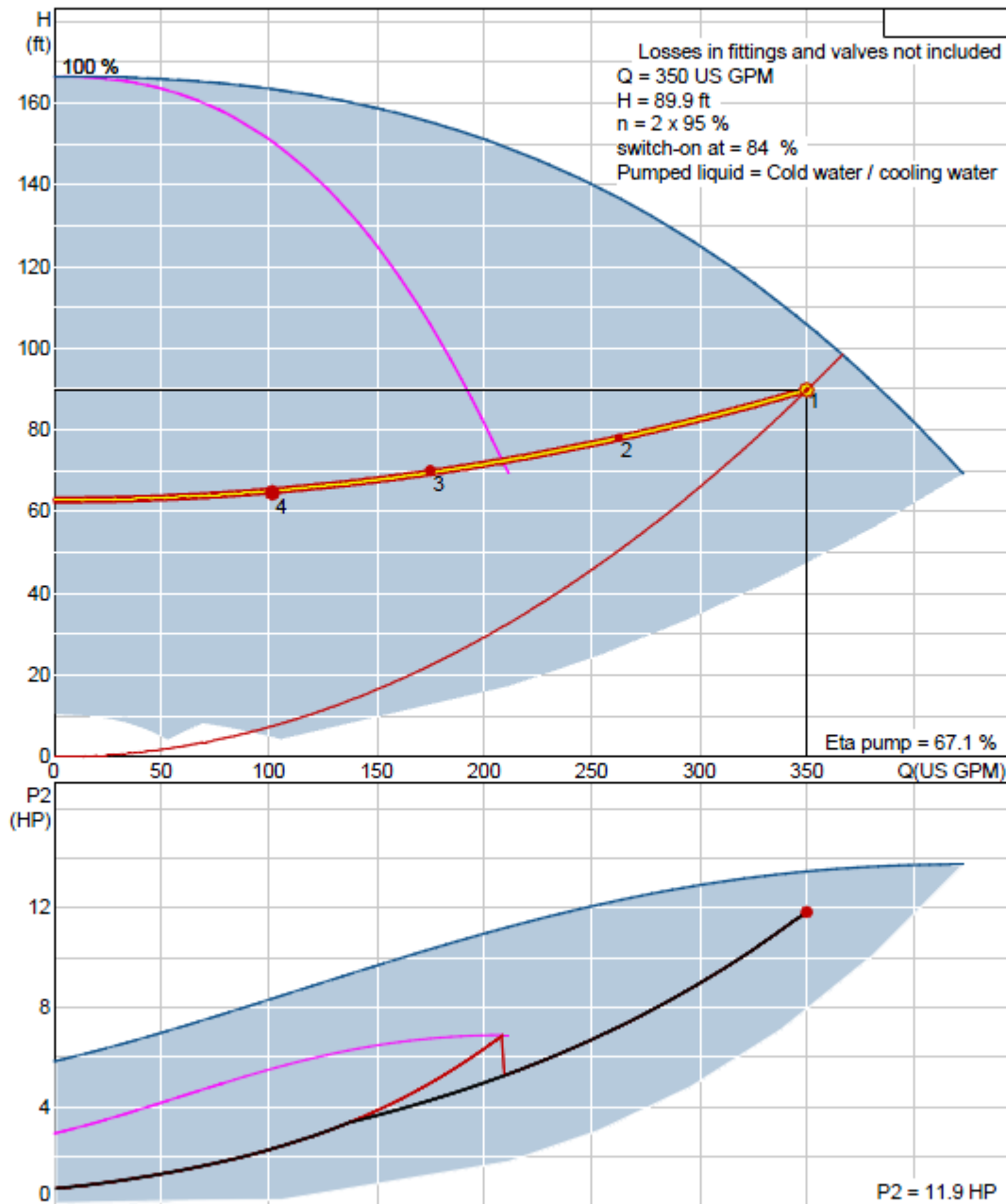
0 267 934

2400

6000 [h]

t





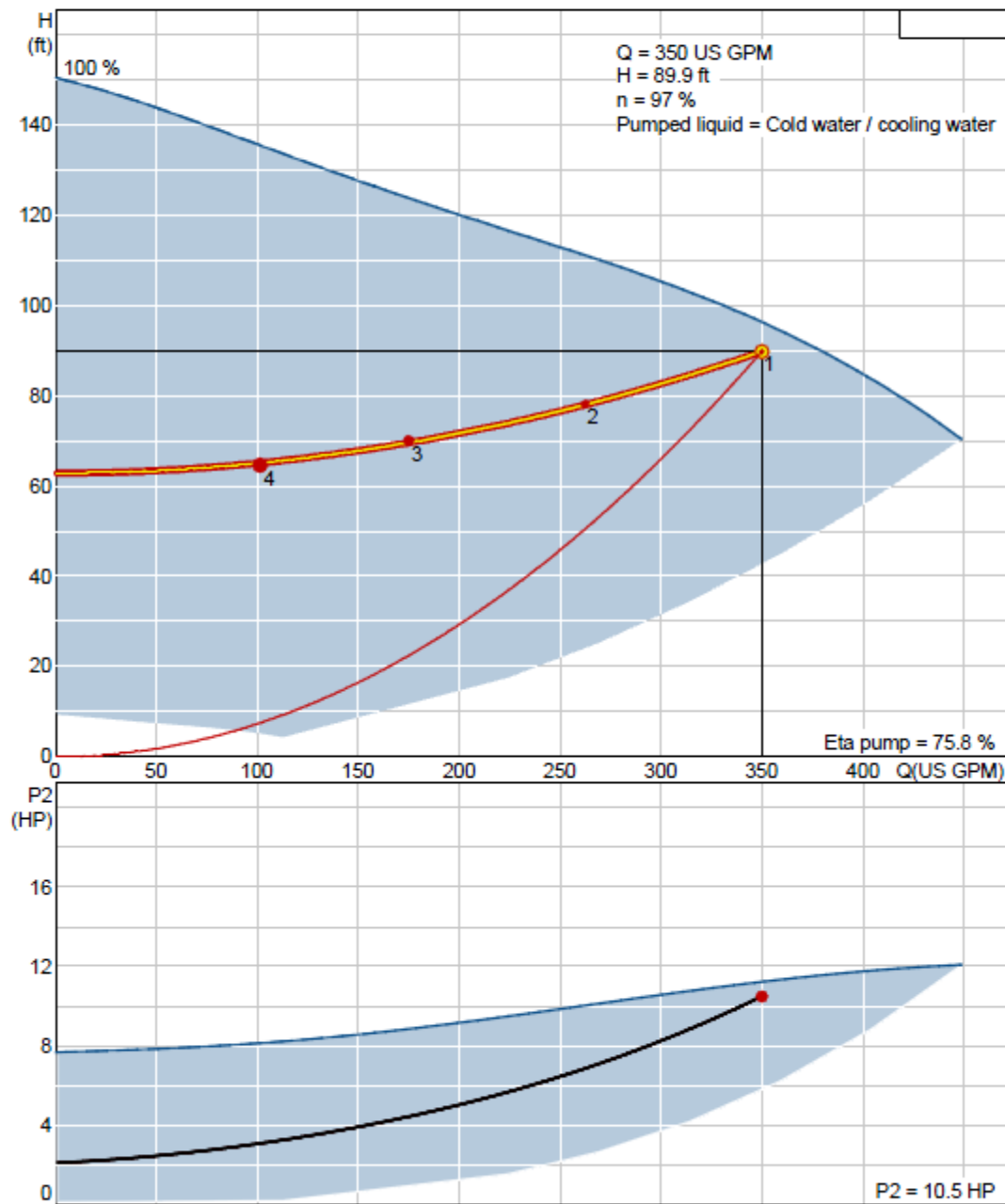
Two 50% pumps:

Design Flow: 350 gpm

Design TDH: 90 feet

Pumps: 2 x 7.5HP

BHP at Design: 11.9



One 100% Pump:

Design Flow: 350 gpm

Design TDH: 90 feet

Pumps: 1 x 15HP

BHP at Design: 10.5

Energy Consumption

1 x 15 HP Pump

Load Profile

	1	2	3	4		
Flow	100	75	50	29	%	
Head	100	87	78	72	%	
P1	9.57	6.28	4.36	3.26	kW	
Time	267	667	1466	3600	h/Year	
Energy consumption	2556	4190	6386	11725	kWh/Year	Total = 24,856 kWh/Year

2 x 7.5 HP Pumps

Load Profile

	1	2	3	4		
Flow	100	75	50	29	%	
Head	100	87	78	72	%	
P1	10.7	6.54	4.08	2.13	kW	
Time	267	667	1466	3600	h/Year	
Energy consumption	2868	4365	5982	7661	kWh/Year	Total = 20,877 kWh/Year
Quantity	2	2	2	1		

At 75-100% flow the single pump has a lower kW requirement (higher pump/motor efficiency). But pumps generally have higher running hours at lower flow rates therefore the two pump solution is a better choice overall due to the higher pump efficiency at flows less than 50%.

Parallel Connected Pumps - Pump Sequencing

Methods:

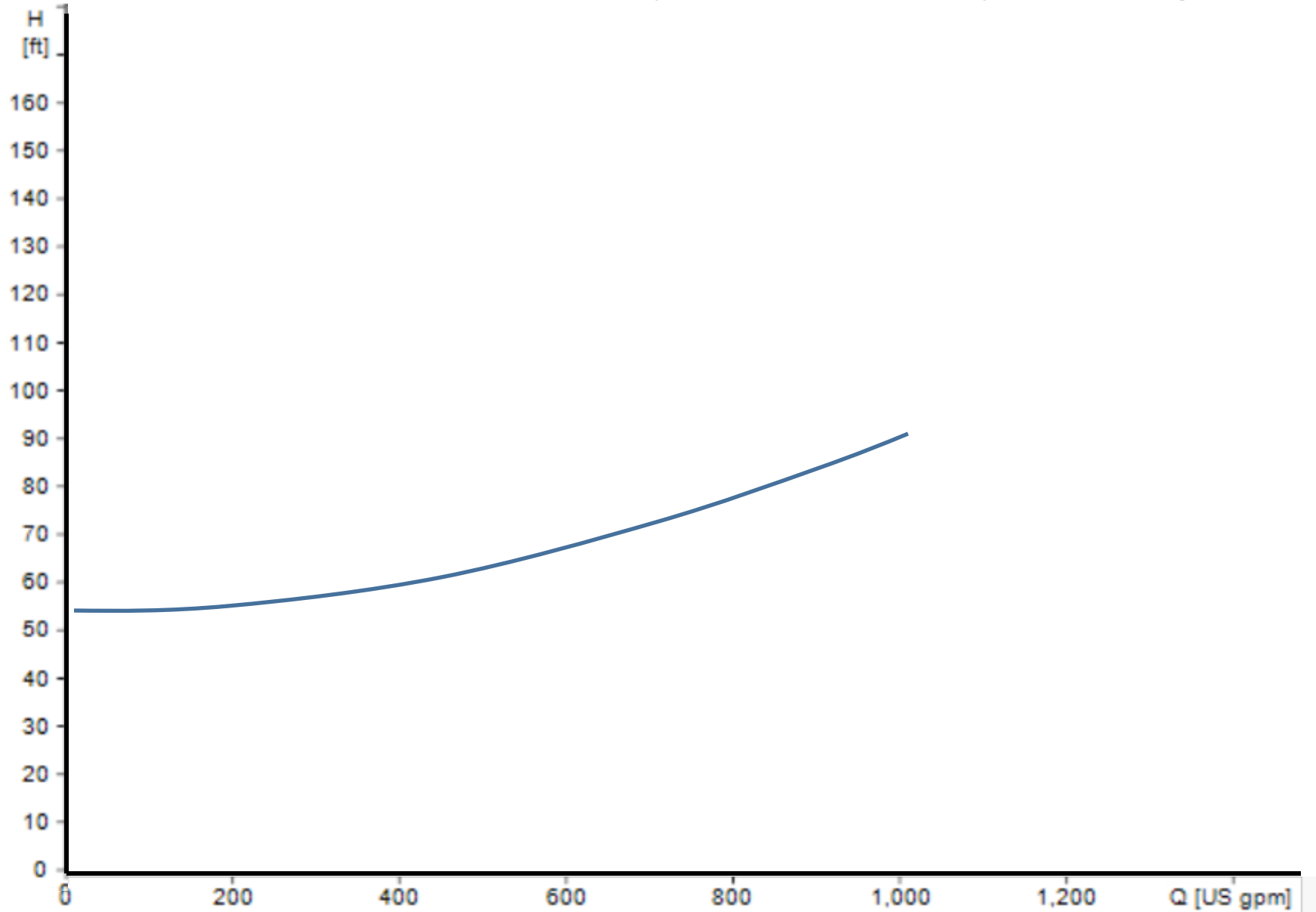
- > Flow
- > Current [Amps]
- > Speed
- > Demand [set-point not being reached]
- > Efficiency

Which is best?

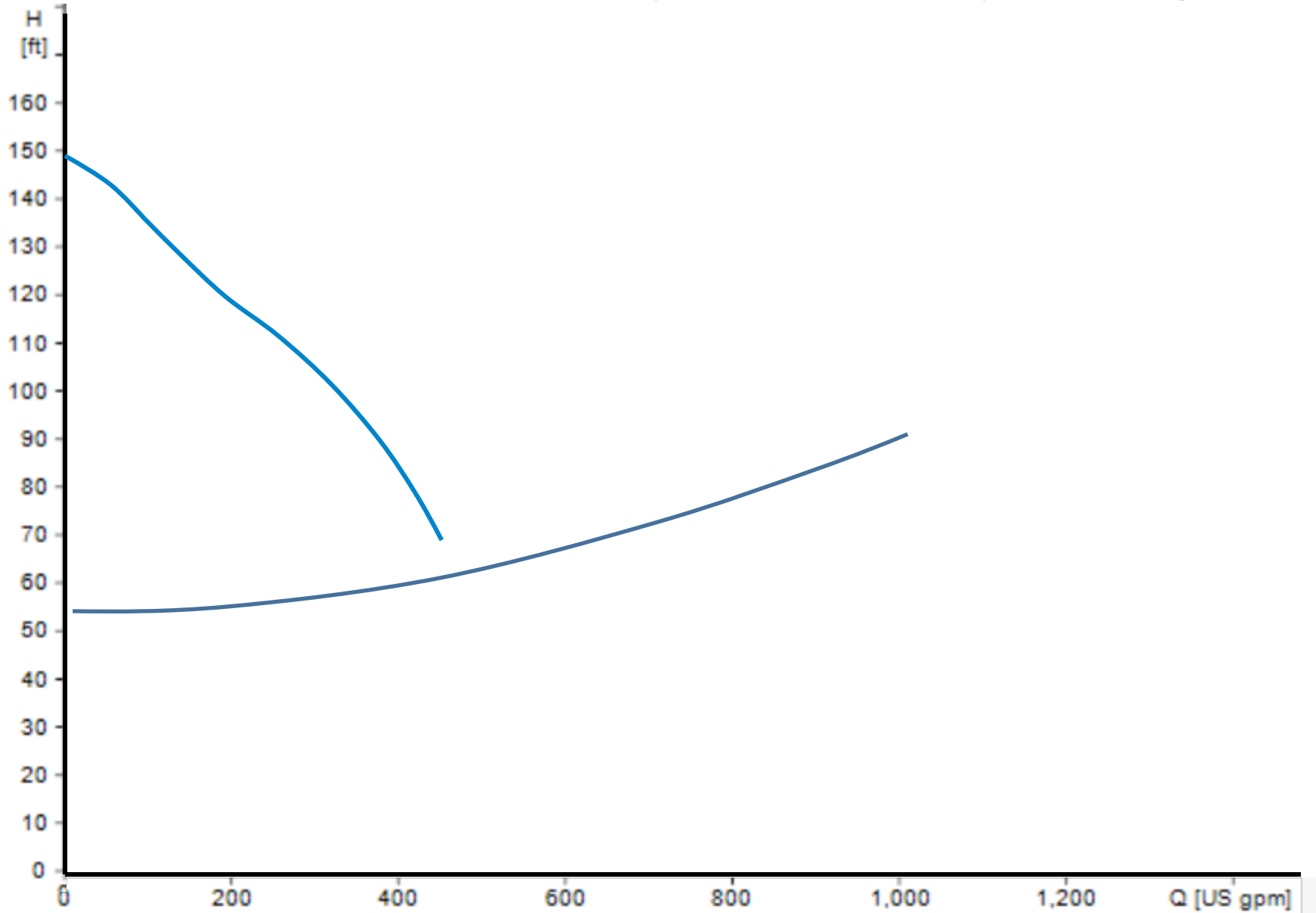
It depends

on a lot of factors

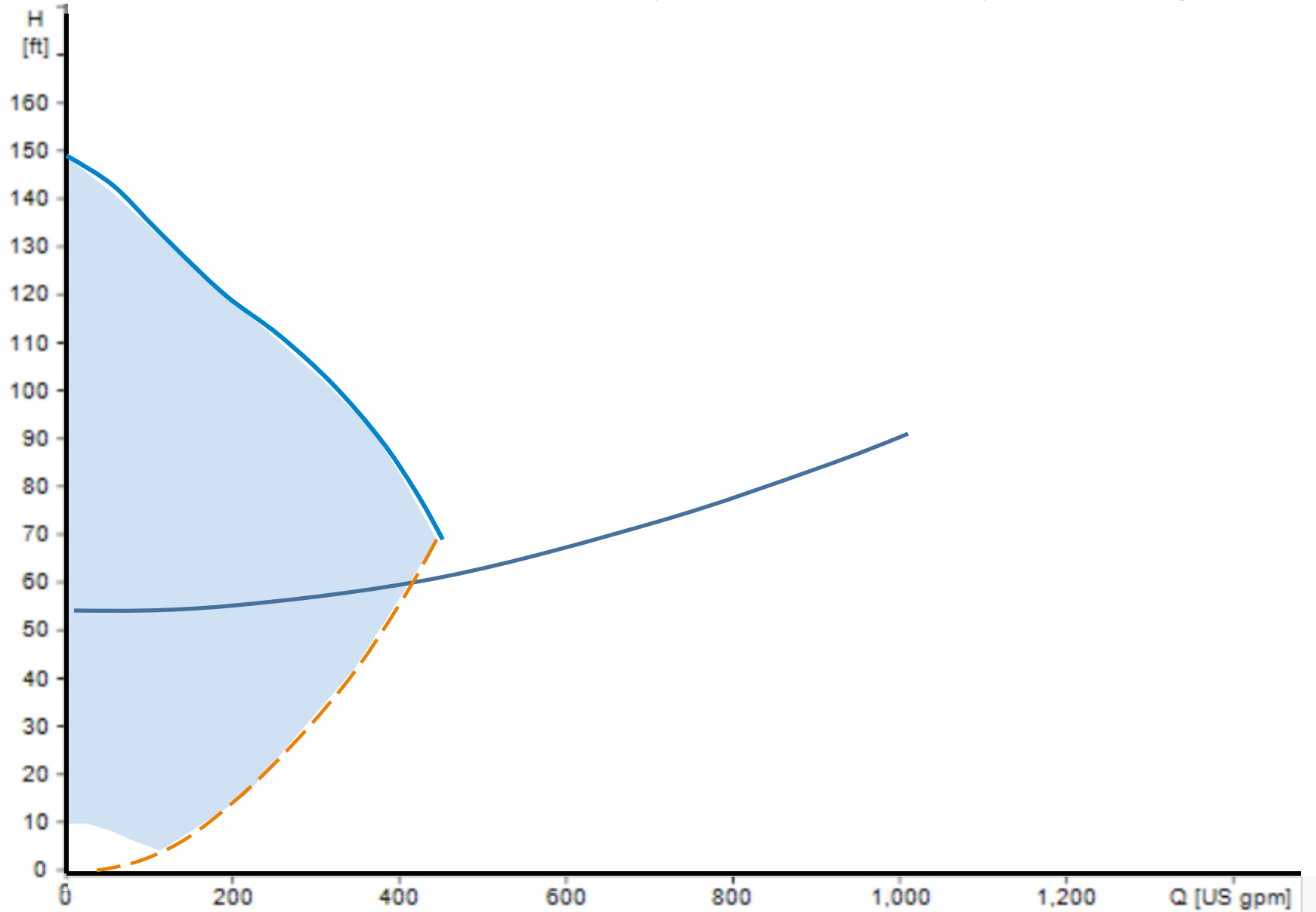
Parallel Connected Pumps - Flow Sequencing



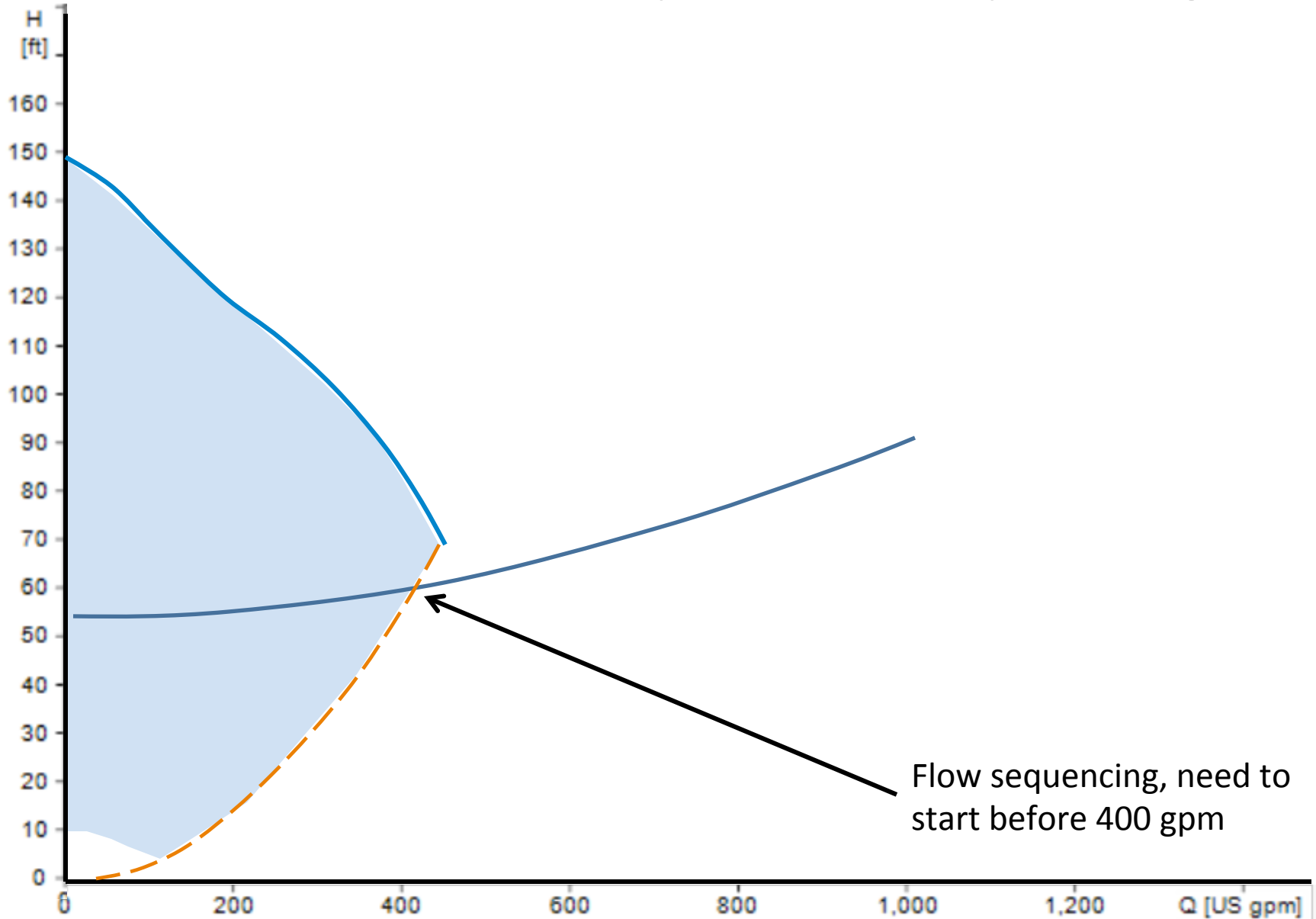
Parallel Connected Pumps - Flow Sequencing



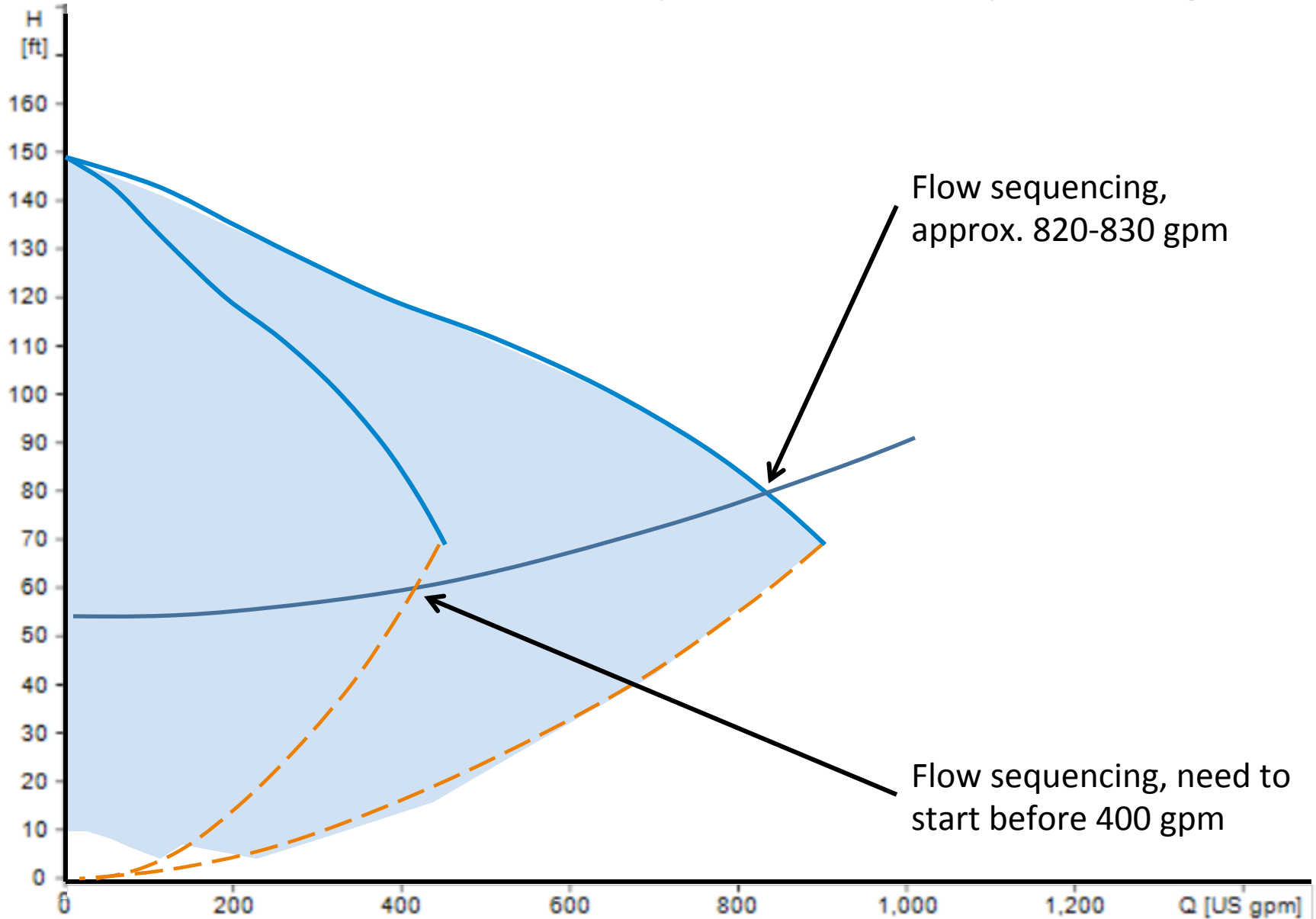
Parallel Connected Pumps - Flow Sequencing



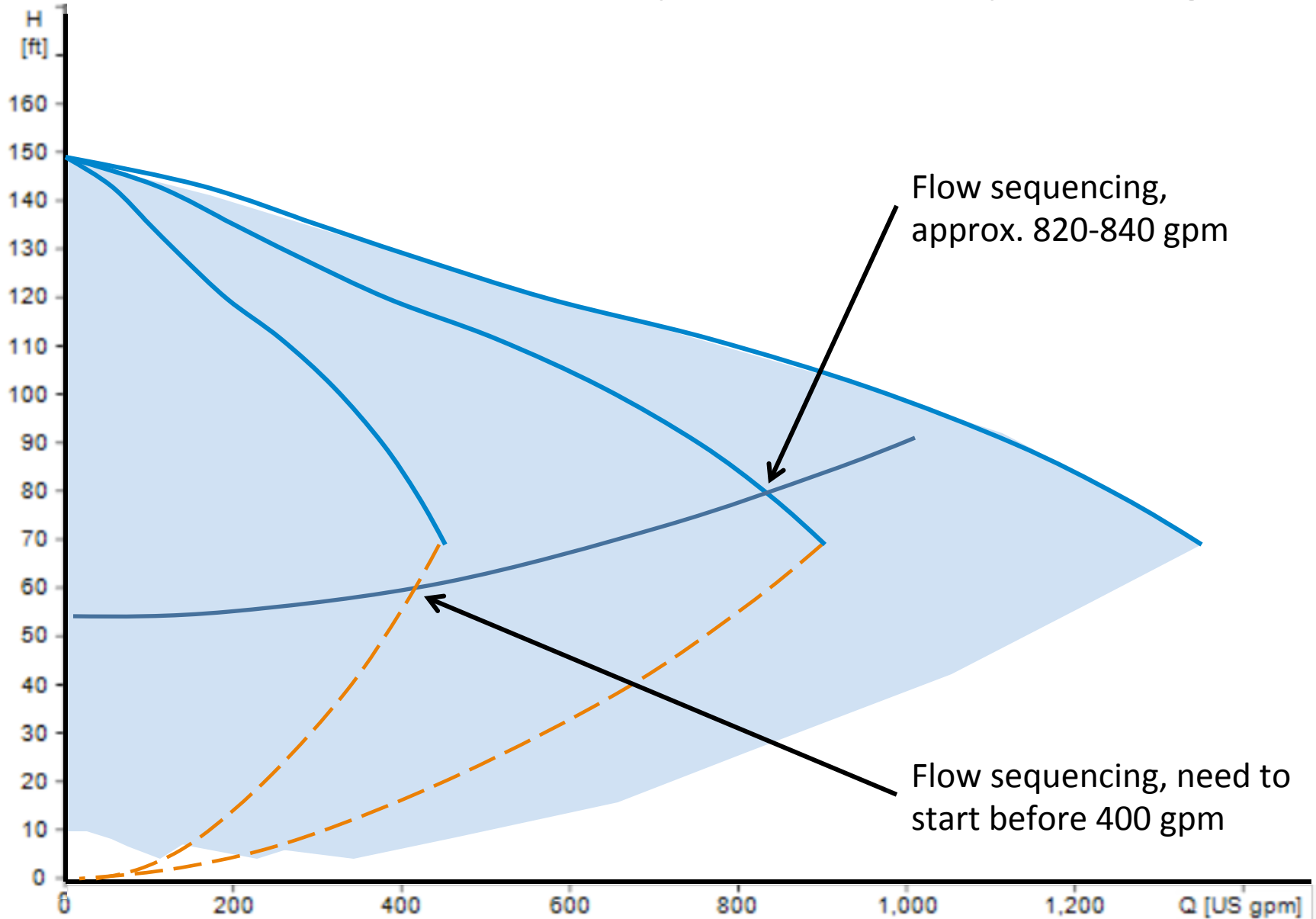
Parallel Connected Pumps - Flow Sequencing



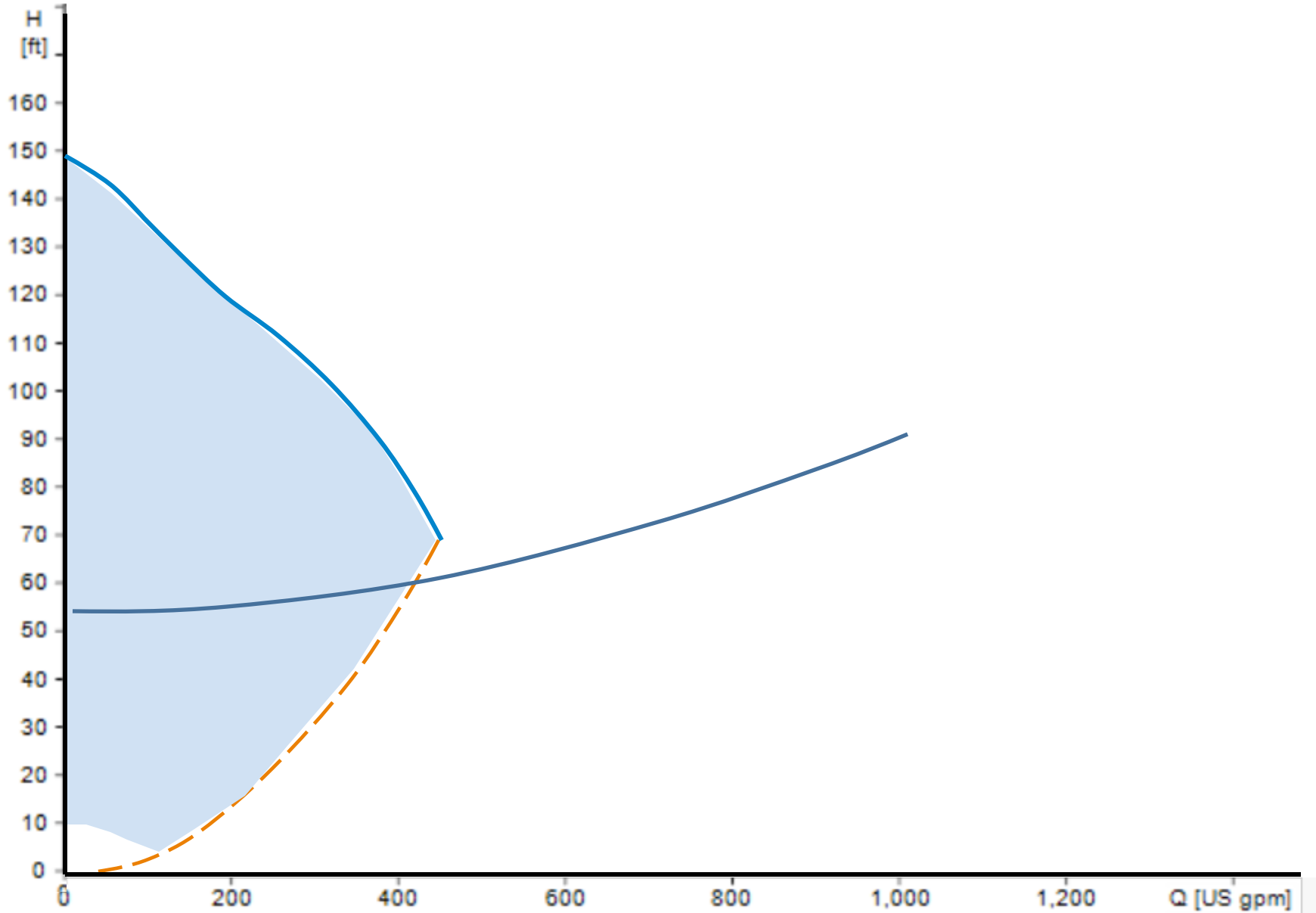
Parallel Connected Pumps - Flow Sequencing



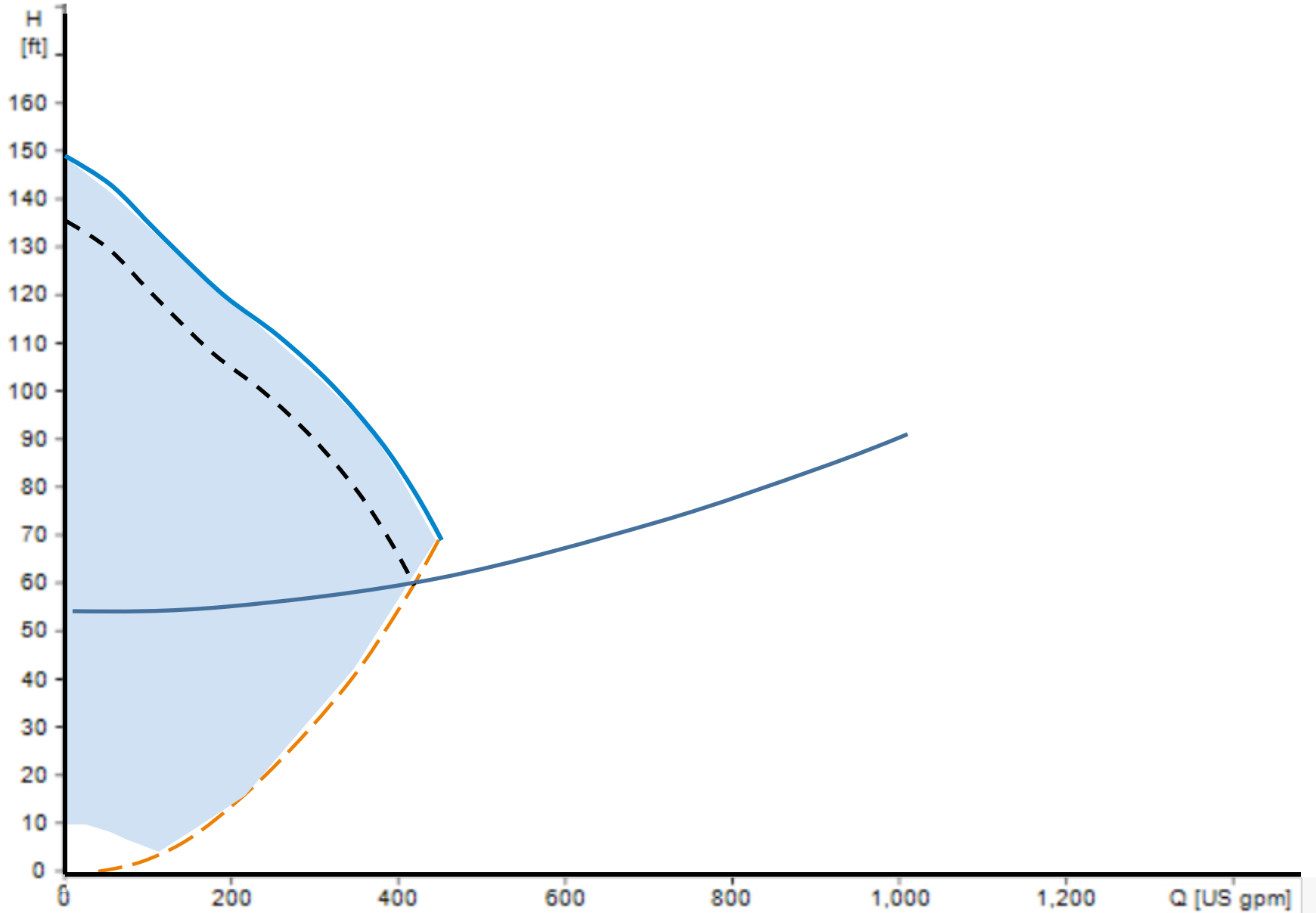
Parallel Connected Pumps - Flow Sequencing



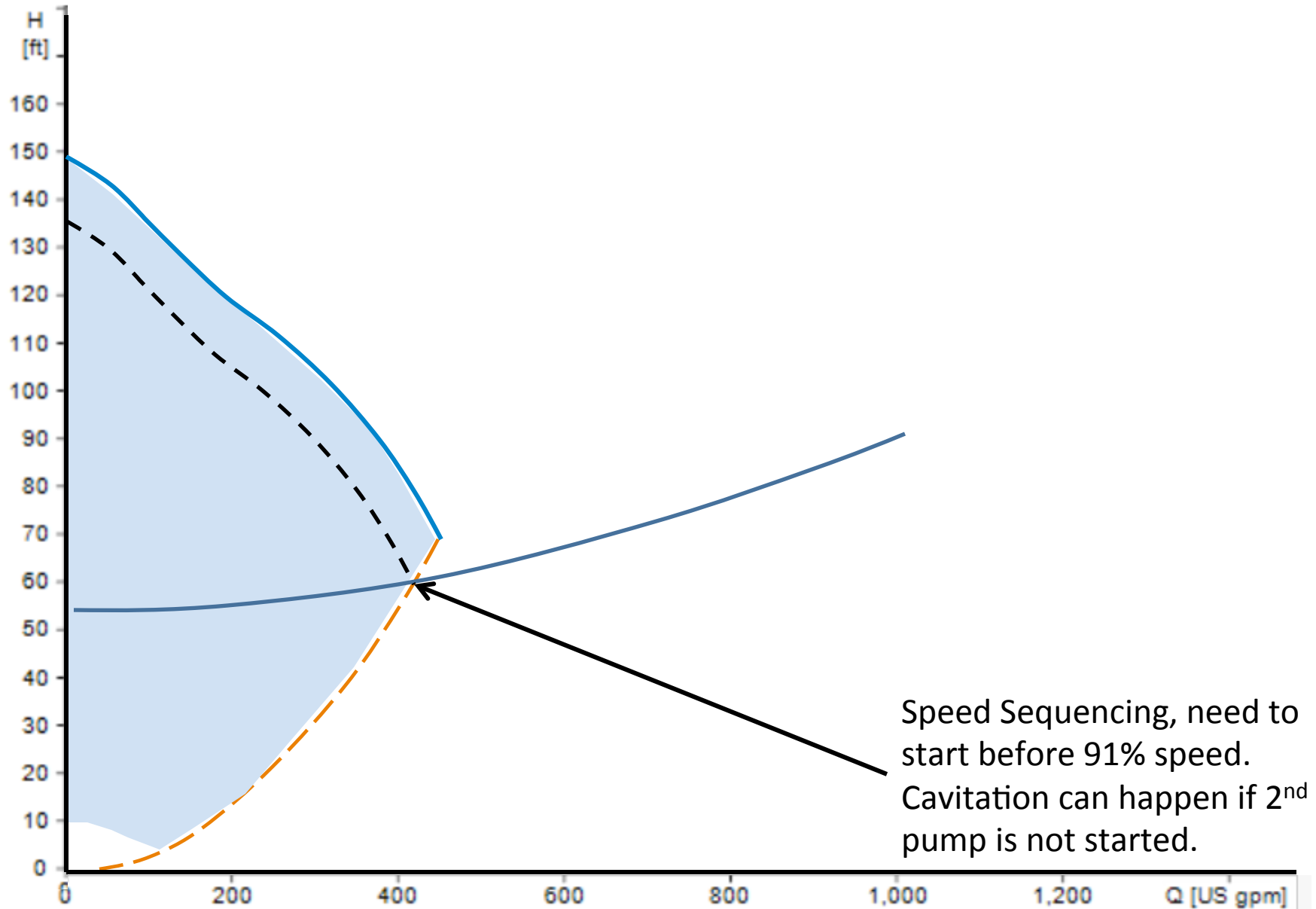
Parallel Connected Pumps – Speed Sequencing



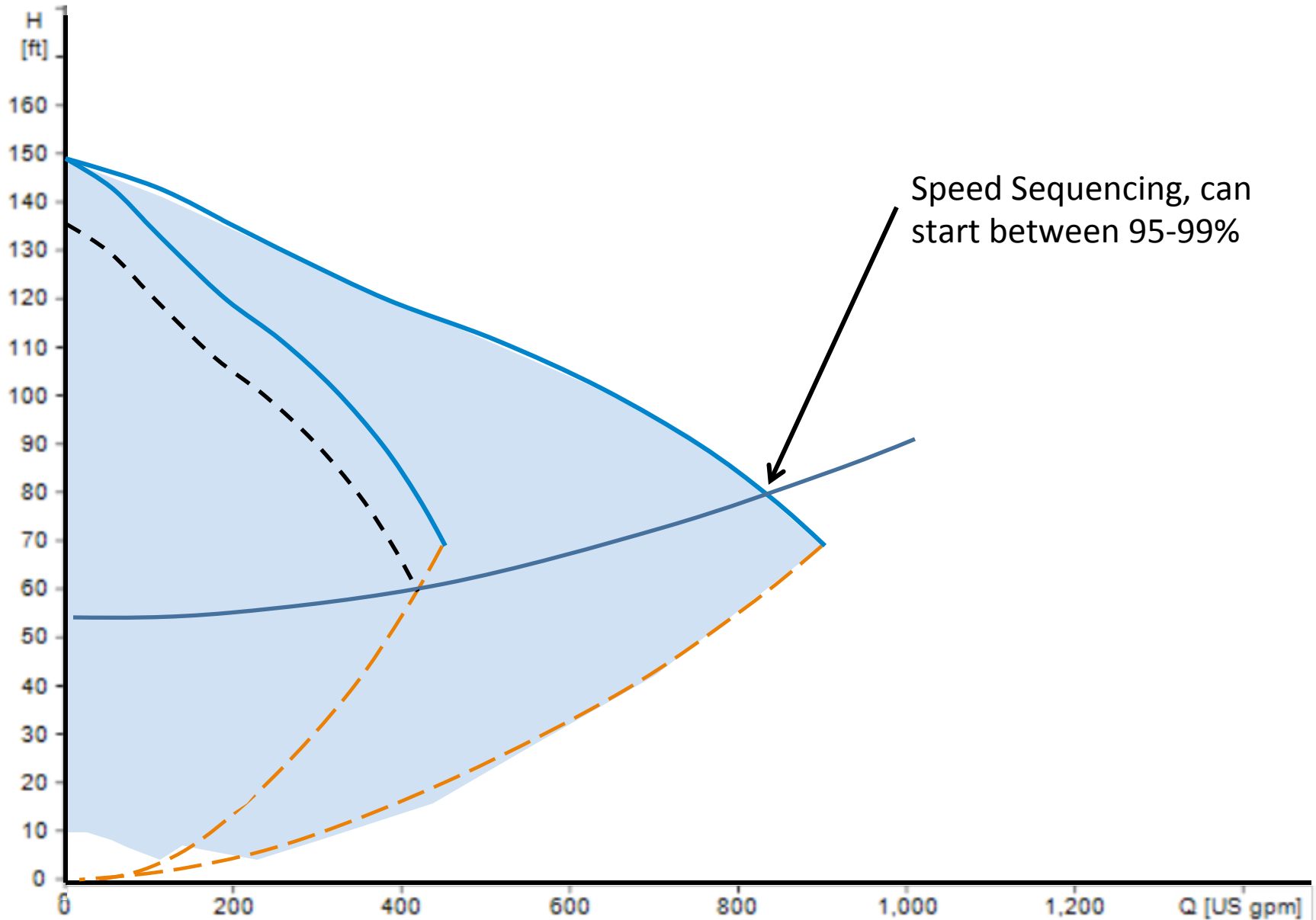
Parallel Connected Pumps – Speed Sequencing



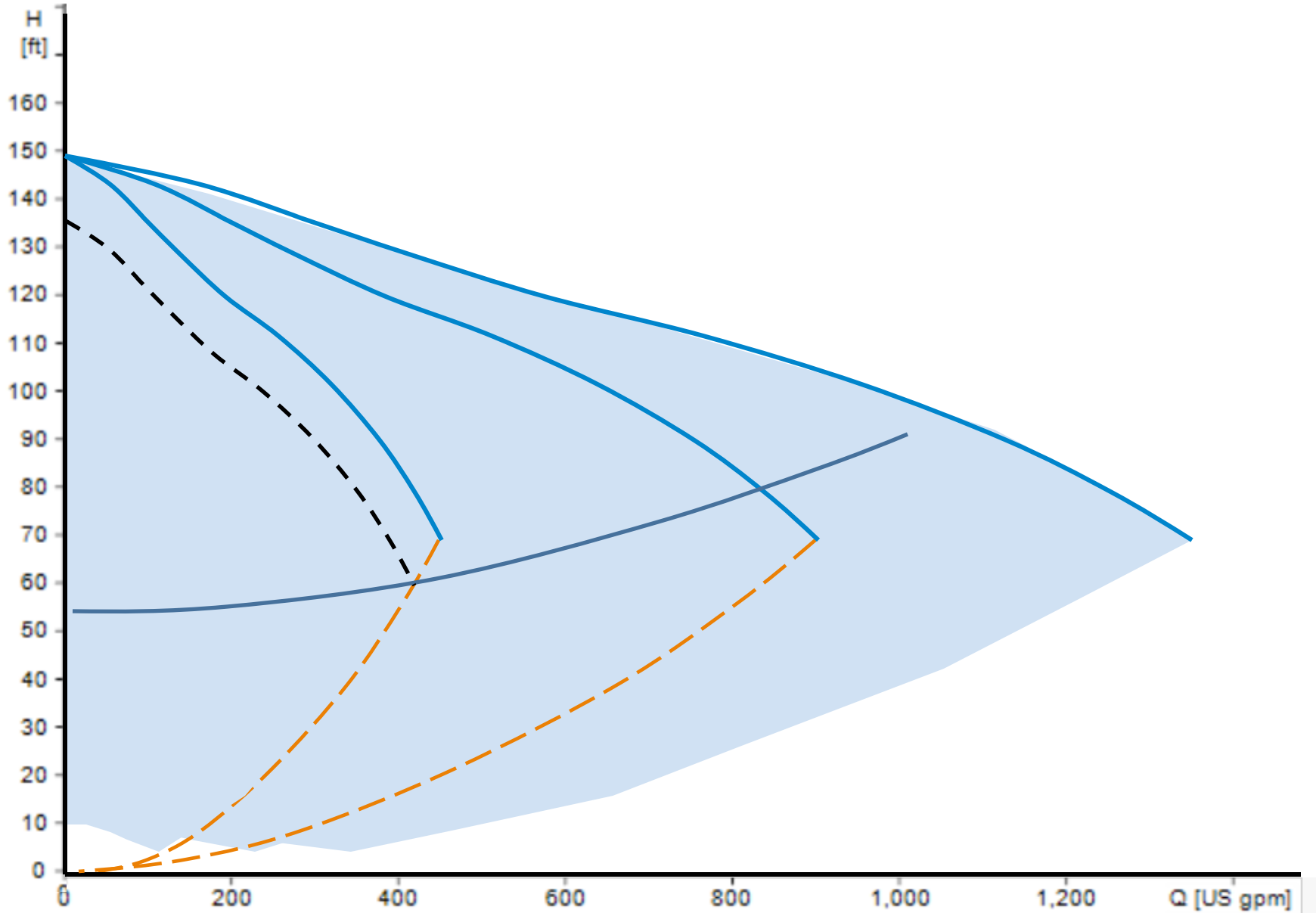
Parallel Connected Pumps – Speed Sequencing



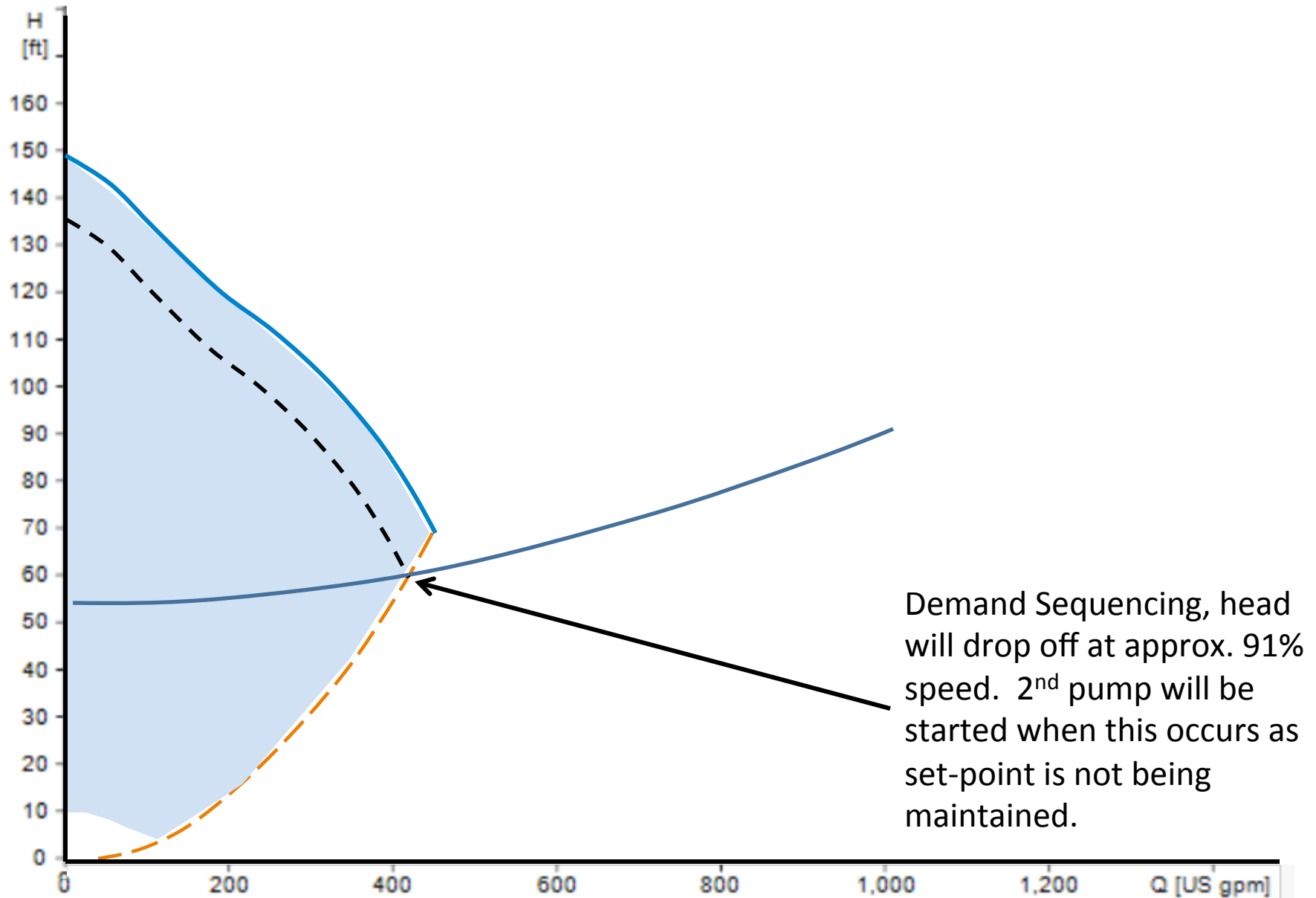
Parallel Connected Pumps – Speed Sequencing



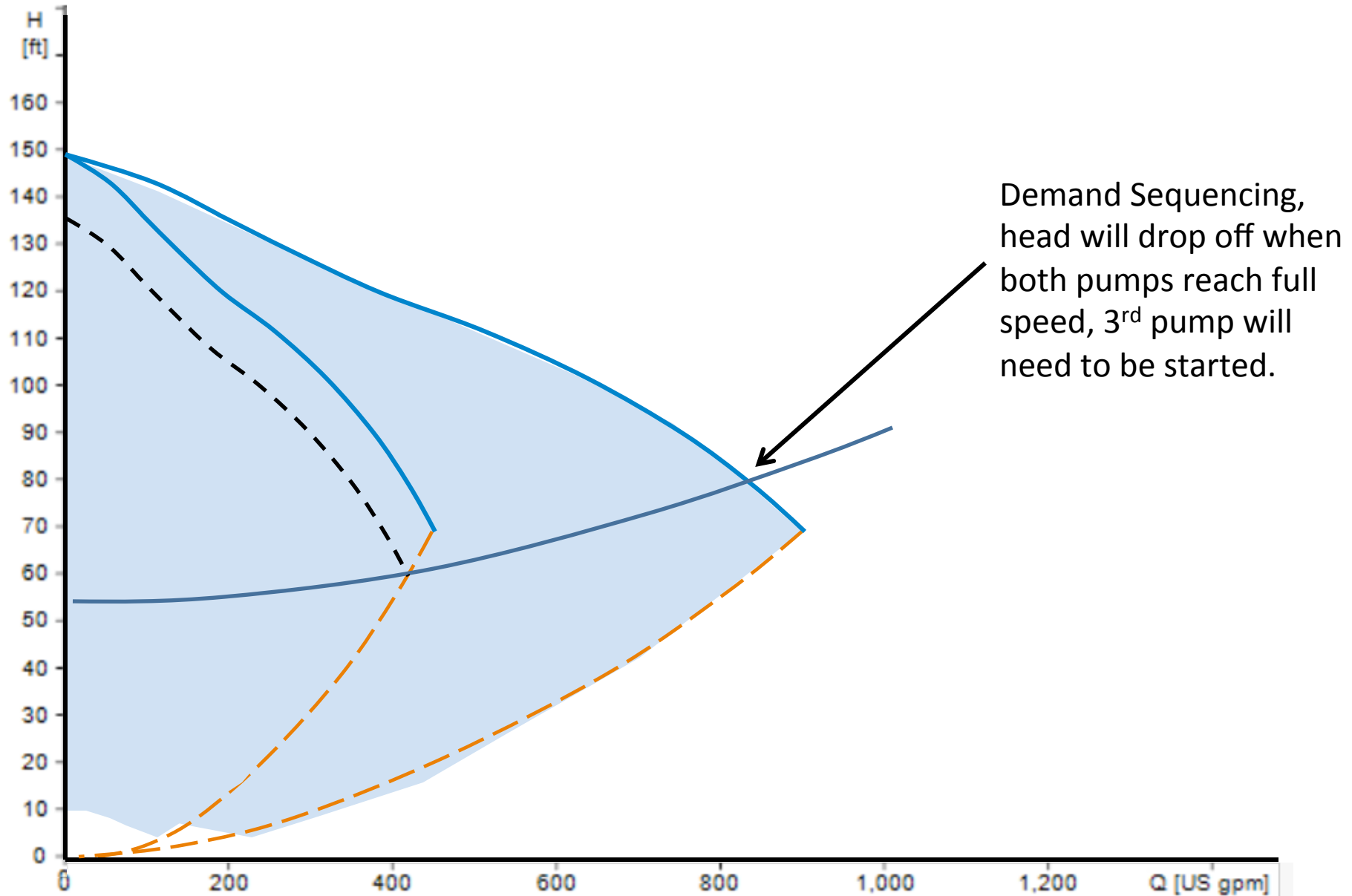
Parallel Connected Pumps – Speed Sequencing



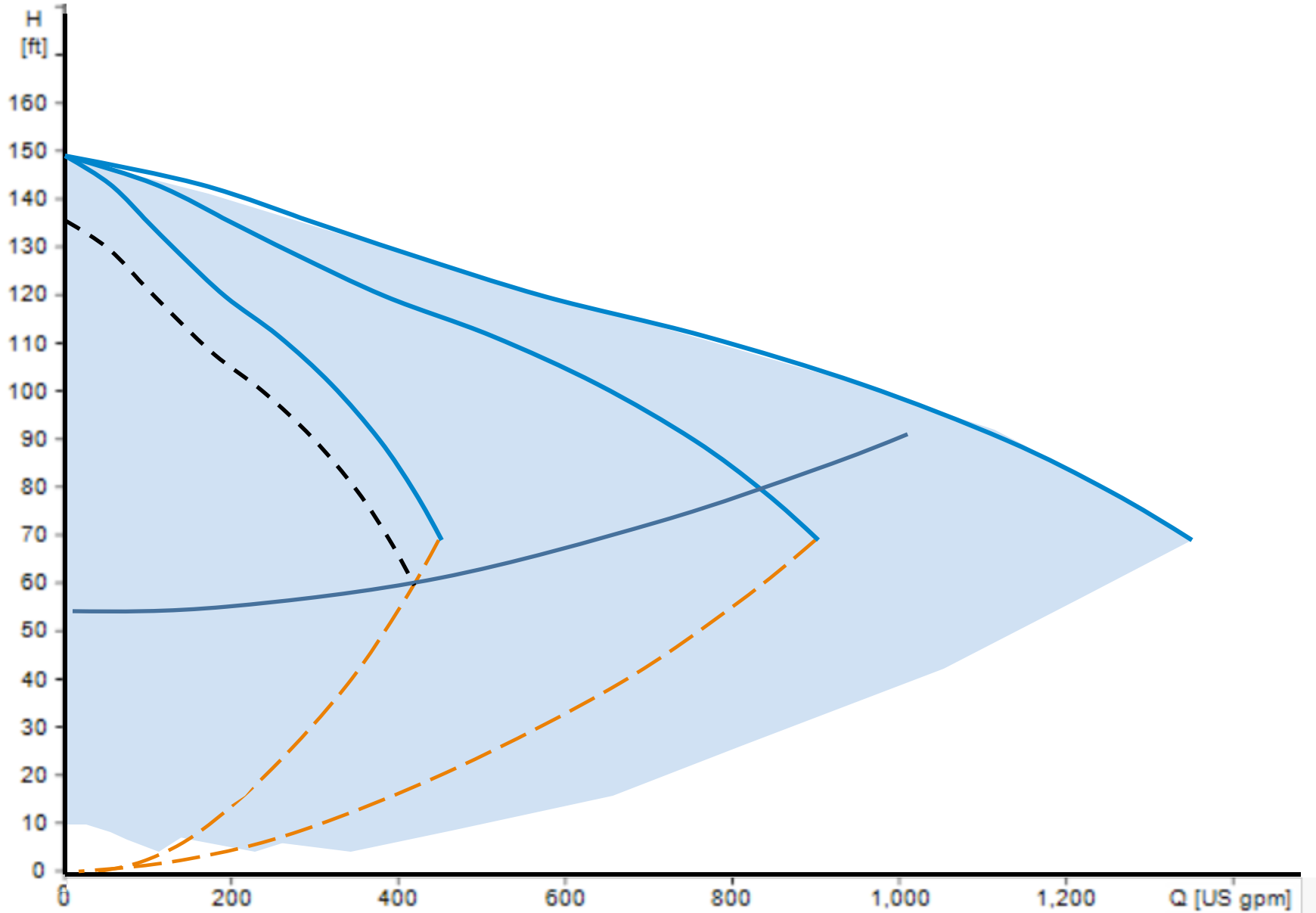
Parallel Connected Pumps – Demand Sequencing



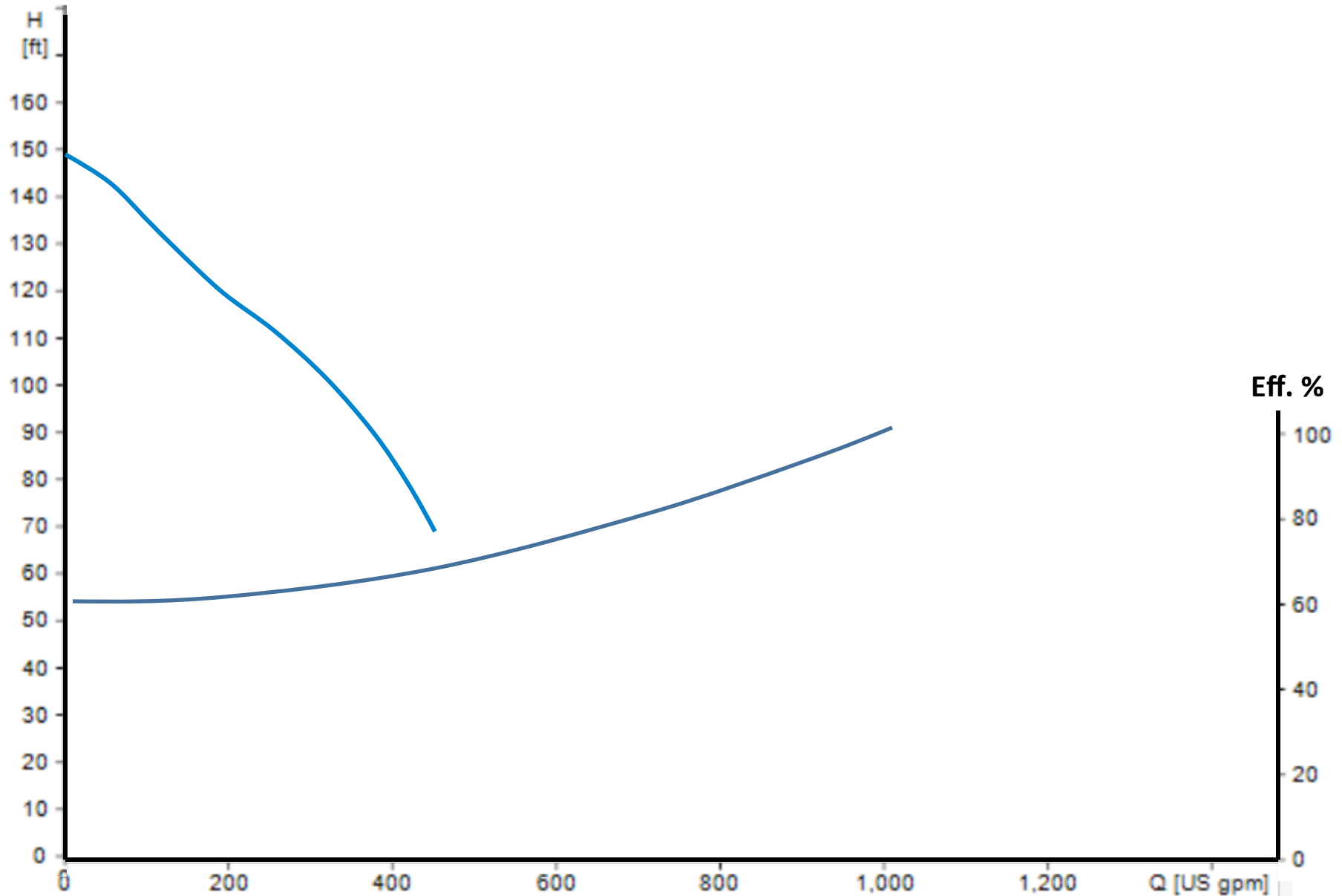
Parallel Connected Pumps – Demand Sequencing



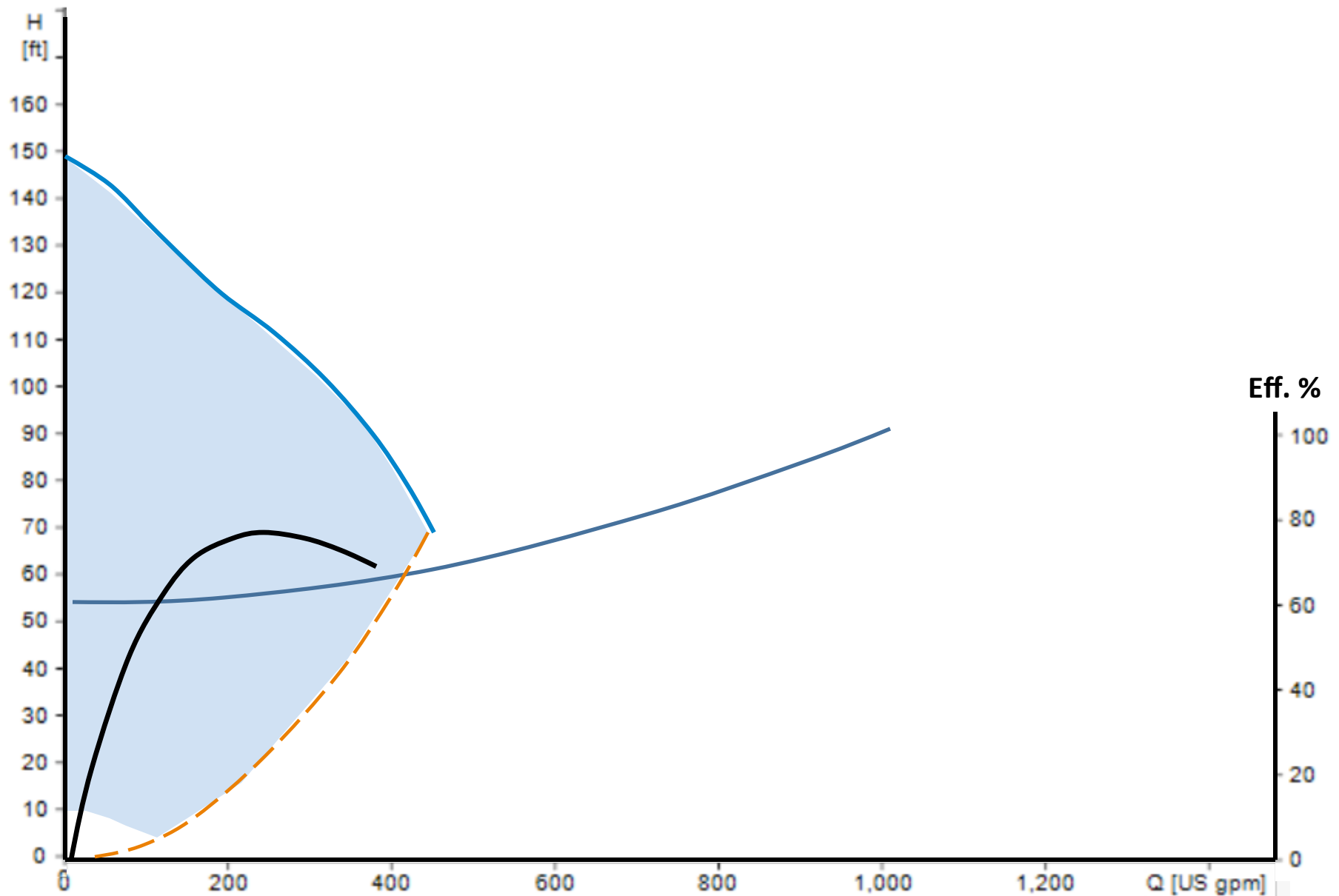
Parallel Connected Pumps – Demand Sequencing



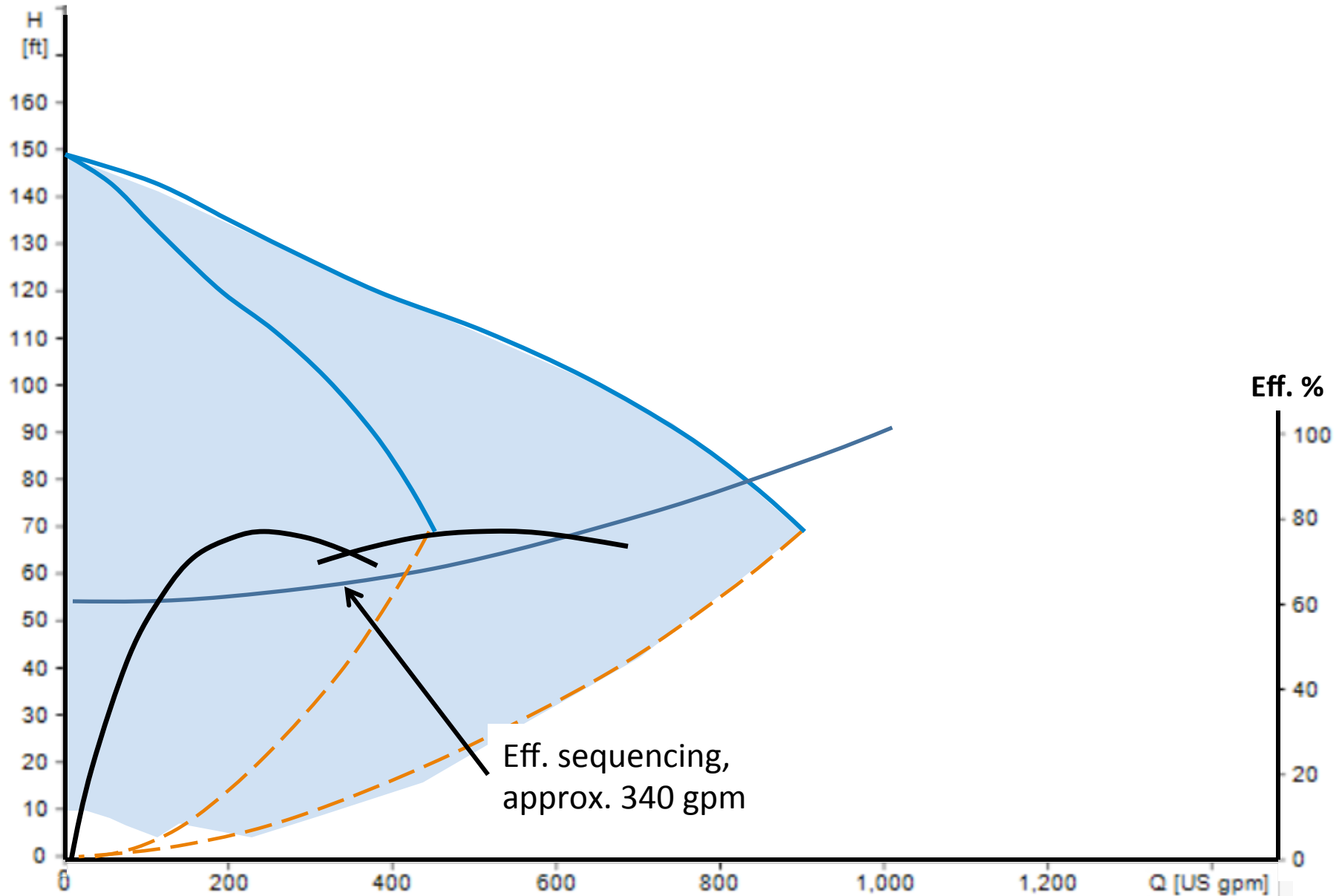
Parallel Connected Pumps - Efficiency Sequencing



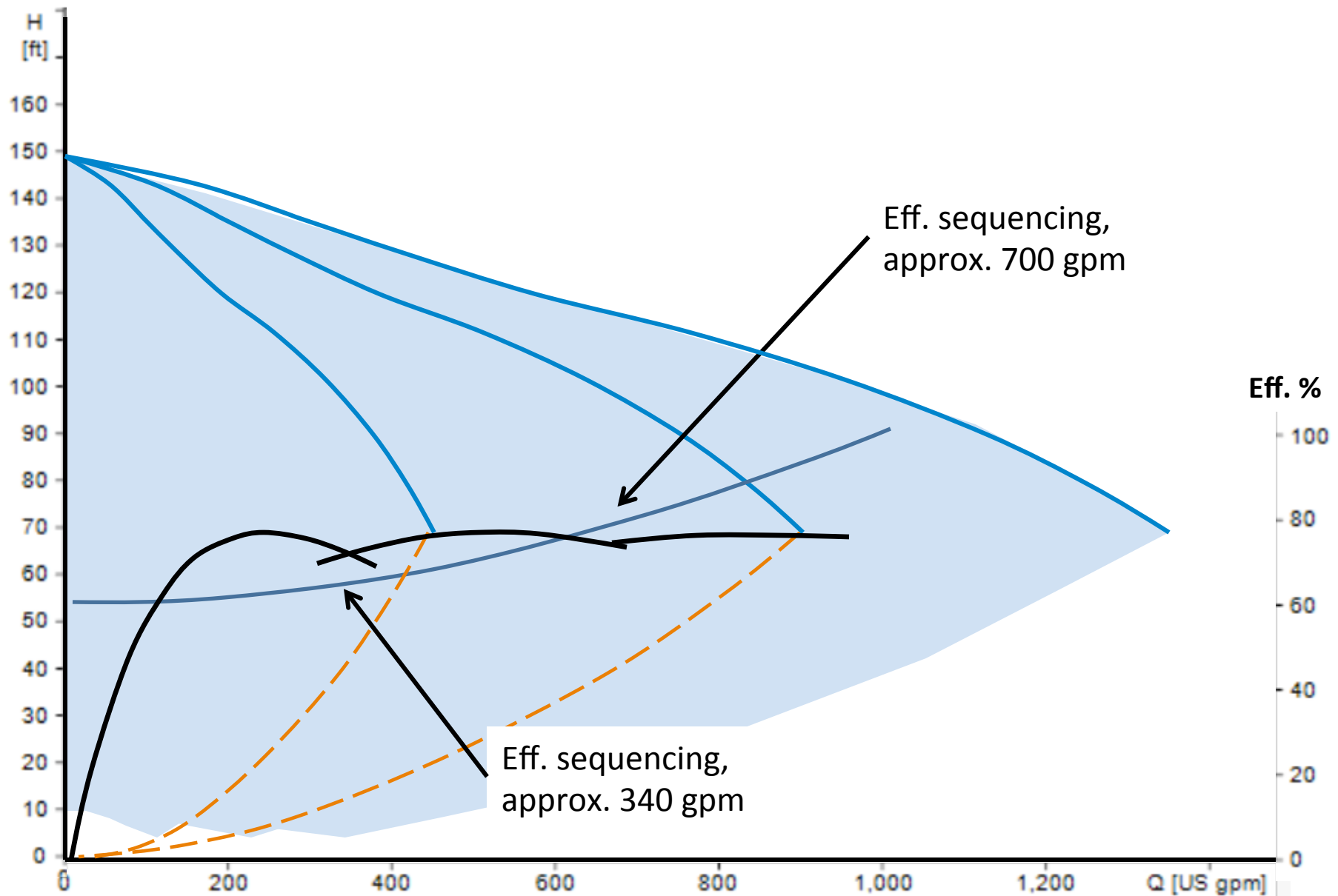
Parallel Connected Pumps - Efficiency Sequencing



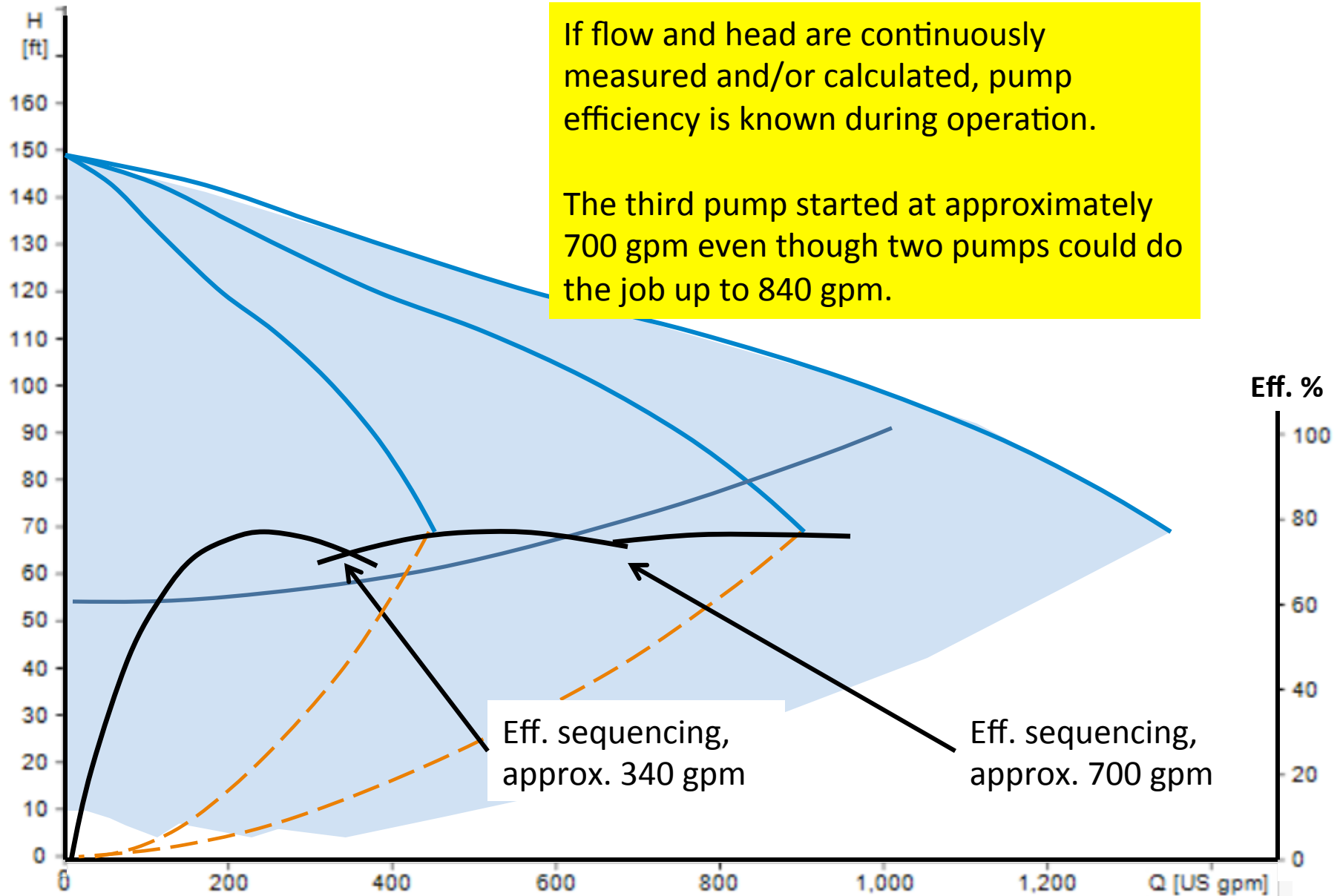
Parallel Connected Pumps - Efficiency Sequencing



Parallel Connected Pumps - Efficiency Sequencing



Parallel Connected Pumps - Efficiency Sequencing



One pump – 400 gpm at 62 feet

$$\text{bhp} = \frac{Q \times H \times \text{SG}}{3960 \times \eta_{\text{pump}}} = \frac{400 \times 62 \times 1.0}{3960 \times 0.683} = 9.2$$

Q = 400 US gpm

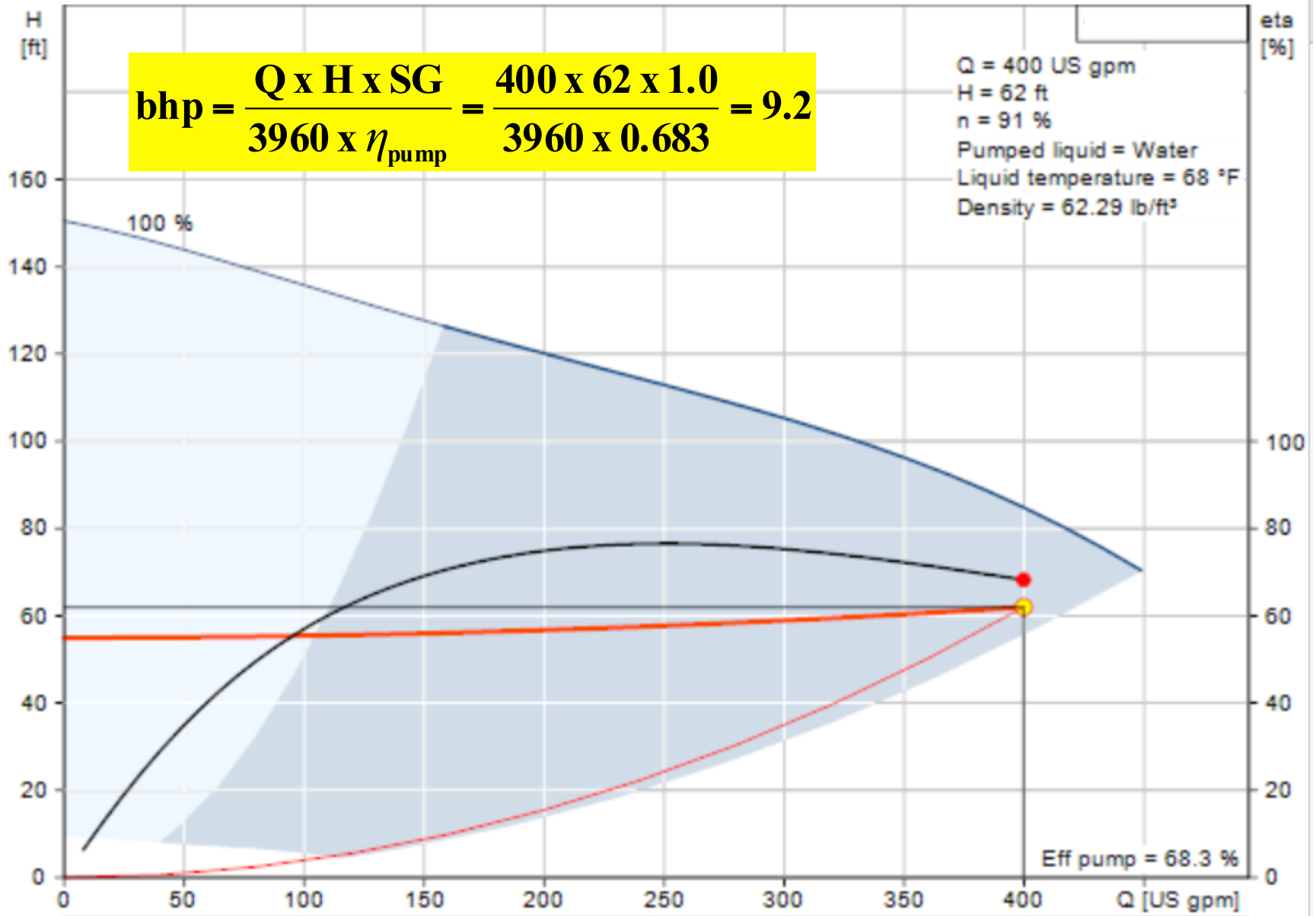
H = 62 ft

n = 91 %

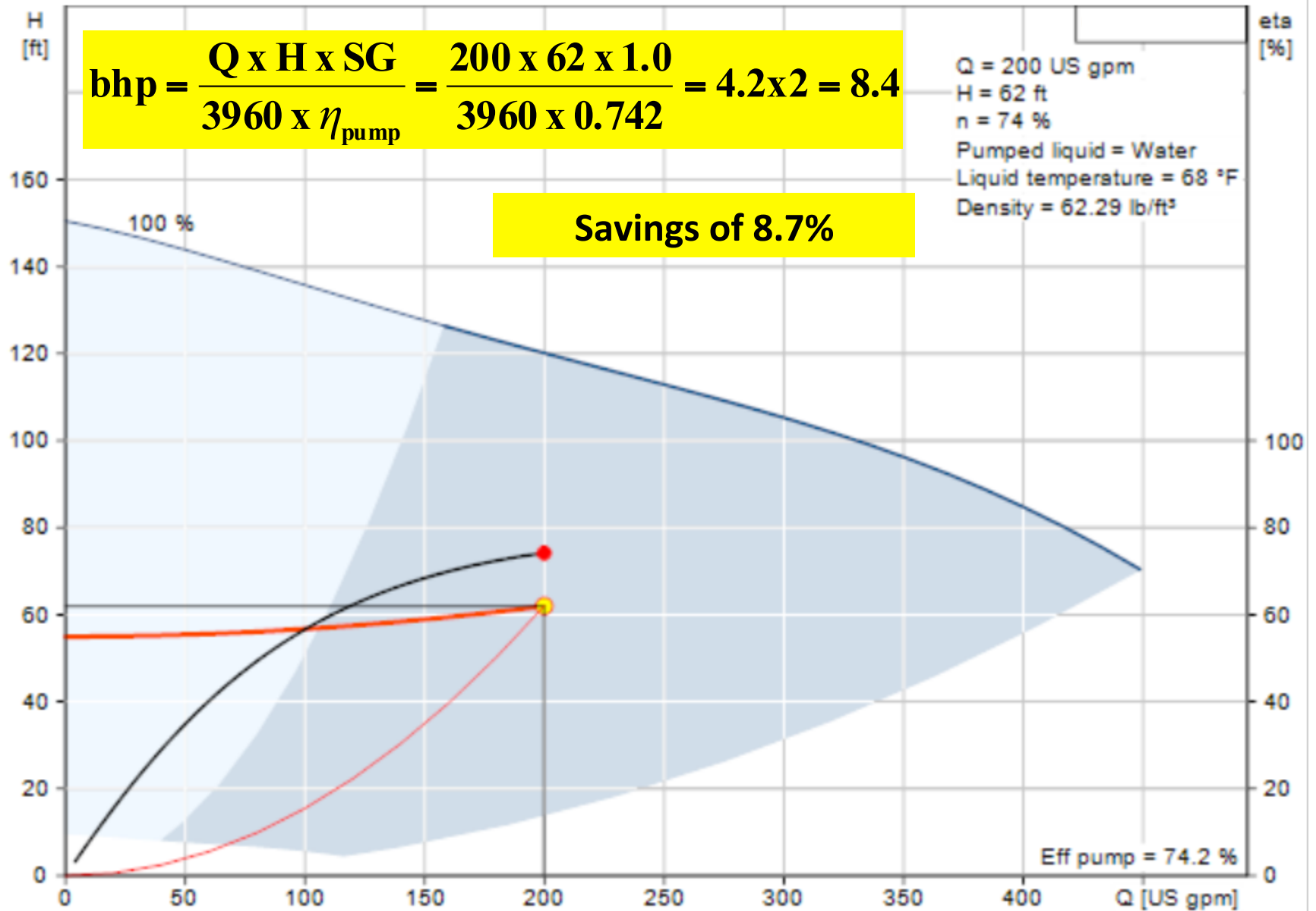
Pumped liquid = Water

Liquid temperature = 68 °F

Density = 62.29 lb/ft³



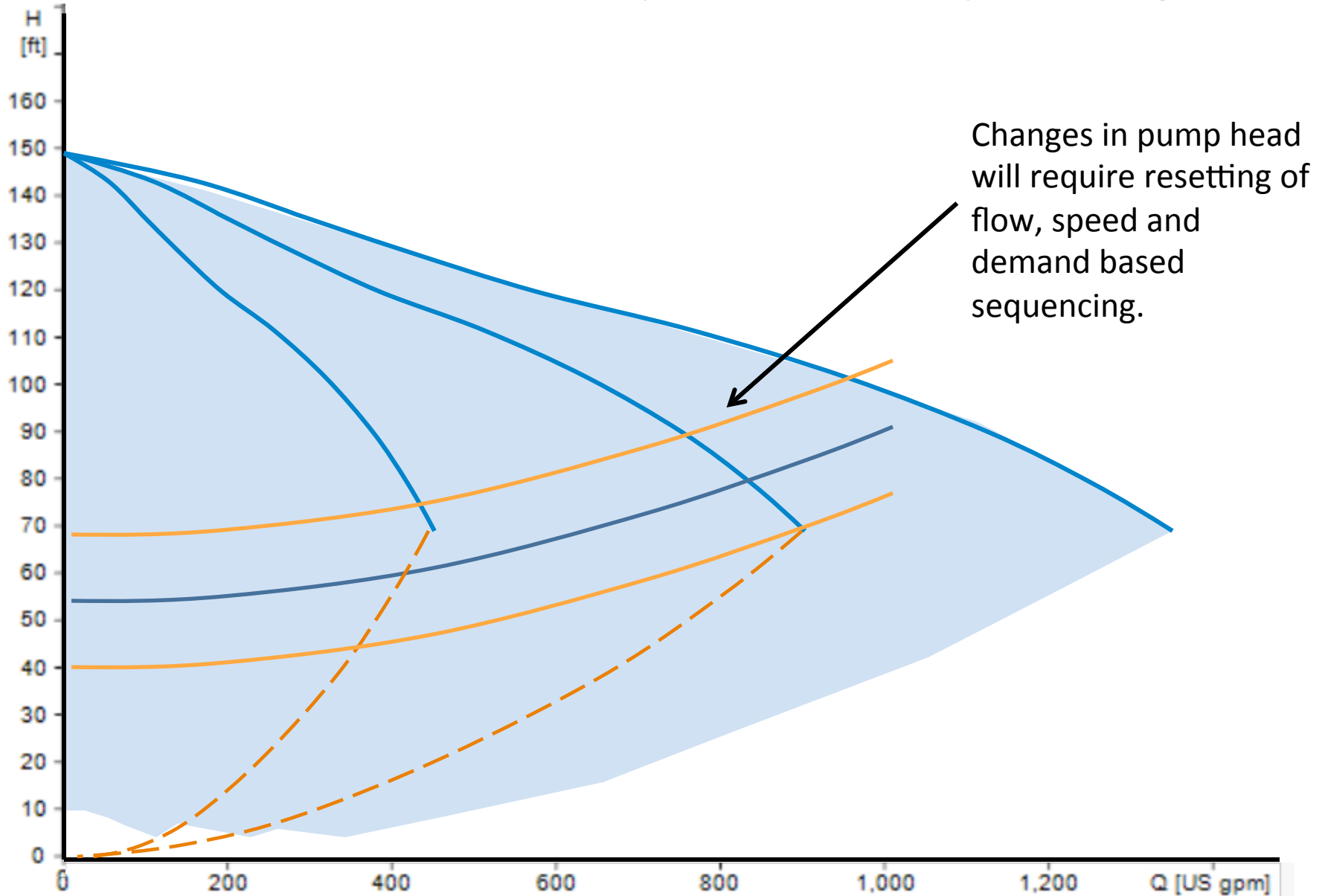
One pump – 200 gpm at 62 feet



What if the required head changes?

Does that effect pump sequencing?

Parallel Connected Pumps - Flow Sequencing



Parallel Connected Pumps - Pump Sequencing

Most efficient: Stage on efficiency

- > Total Efficiency (Electrical + Hydraulic)

- > Hydraulic Efficiency

Parallel Connected Pumps - Pump Sequencing

Most efficient: Stage on efficiency

- > Total Efficiency (Electrical + Hydraulic)
- > Hydraulic Efficiency

Exception

- > Limited suction head, must start additional pumps before flow gets too high

Examples: Boiler Feed, Cooling Tower, water supply from break tank

Grundfos Technical Institute



Thank you for your attention!

www.grundfos.us/training

NOTE:

The following slides are not part of main slide deck but are left here just in case they can be used to help the Q&A session. If the presentation is made available to the viewers, these slide are to be **LEFT OUT**.

Misconception

Since variable head losses are such a small percentage of the total head in high rise building applications, variable frequency drives result in little or no energy savings.

Sample Multi-Stage

A = 25 gpm at 180 feet TDH, 2882 rpm, bhp = 2.3

B = 25 gpm at 266 feet TDH, 3500 rpm, bhp = 3.9

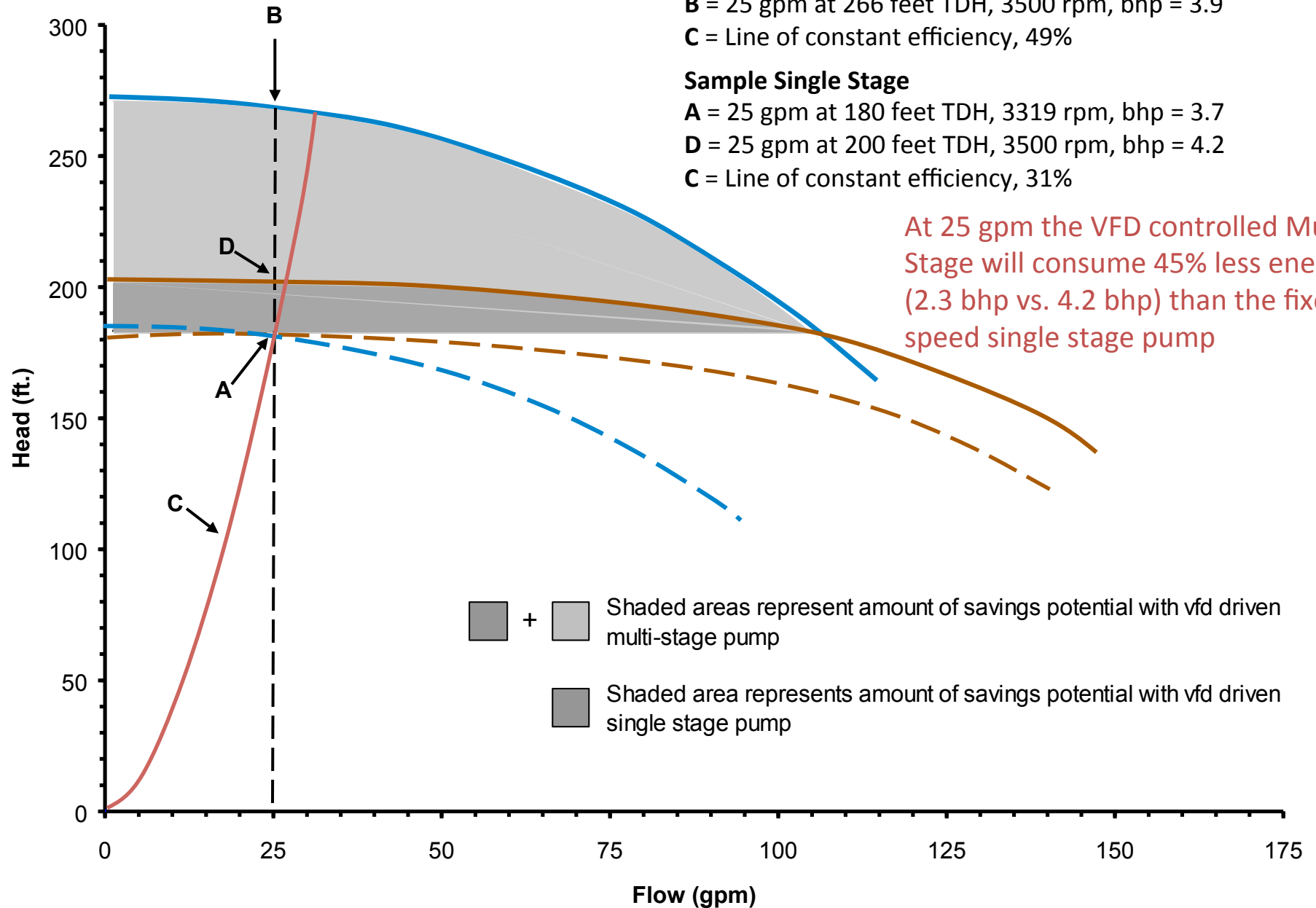
C = Line of constant efficiency, 49%

Sample Single Stage

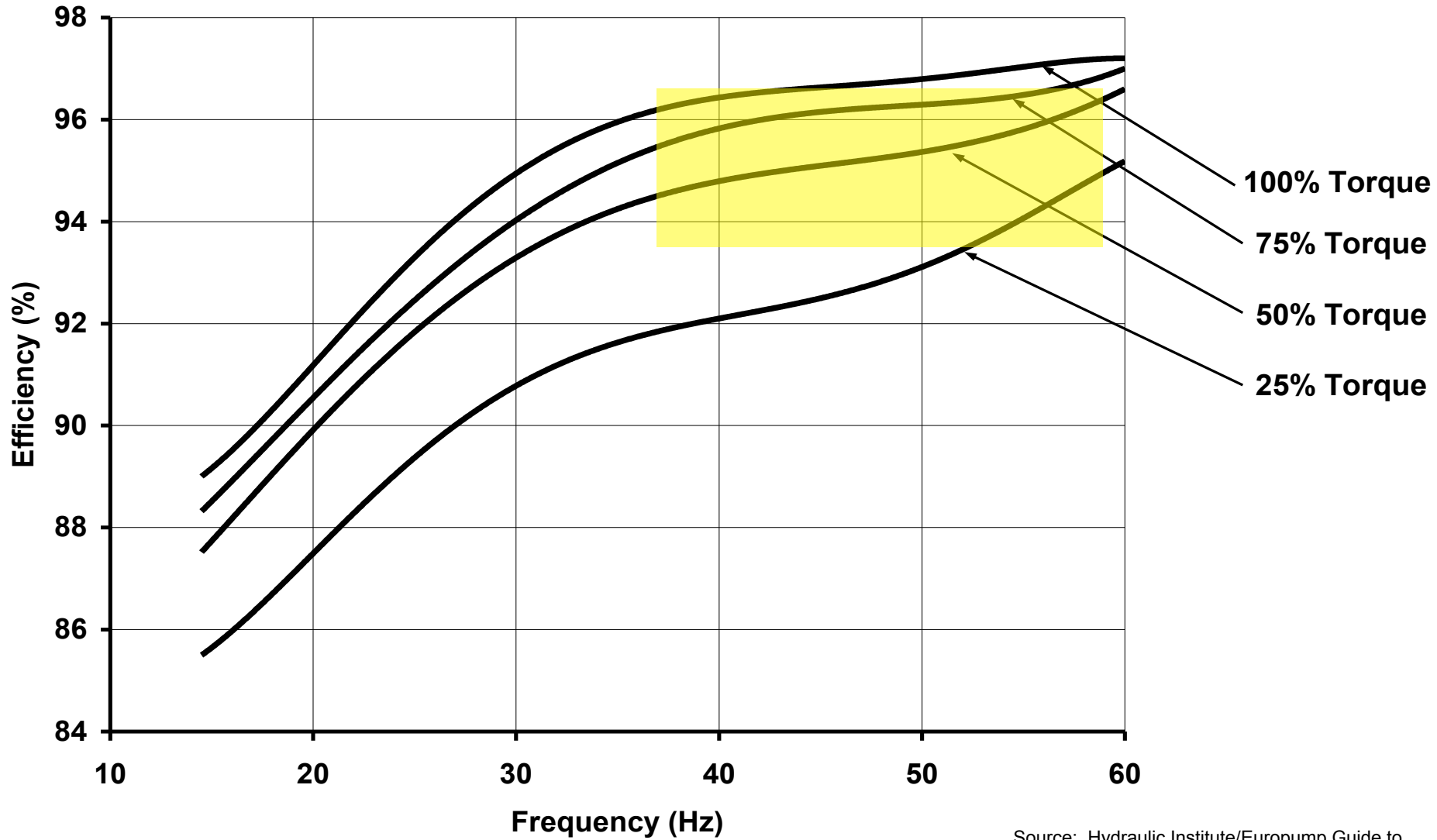
A = 25 gpm at 180 feet TDH, 3319 rpm, bhp = 3.7

D = 25 gpm at 200 feet TDH, 3500 rpm, bhp = 4.2

C = Line of constant efficiency, 31%

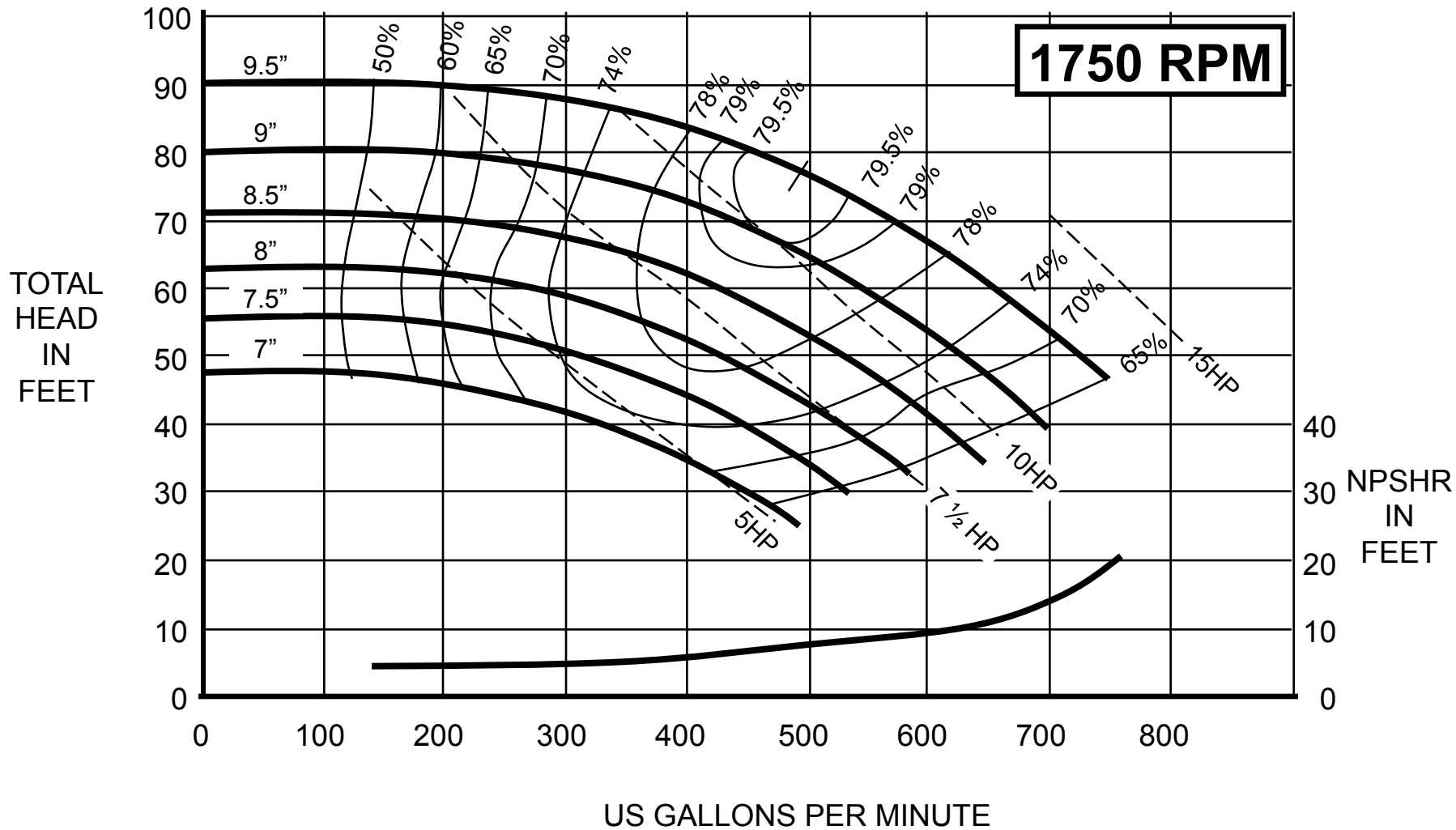


Typical VFD Efficiency Curve

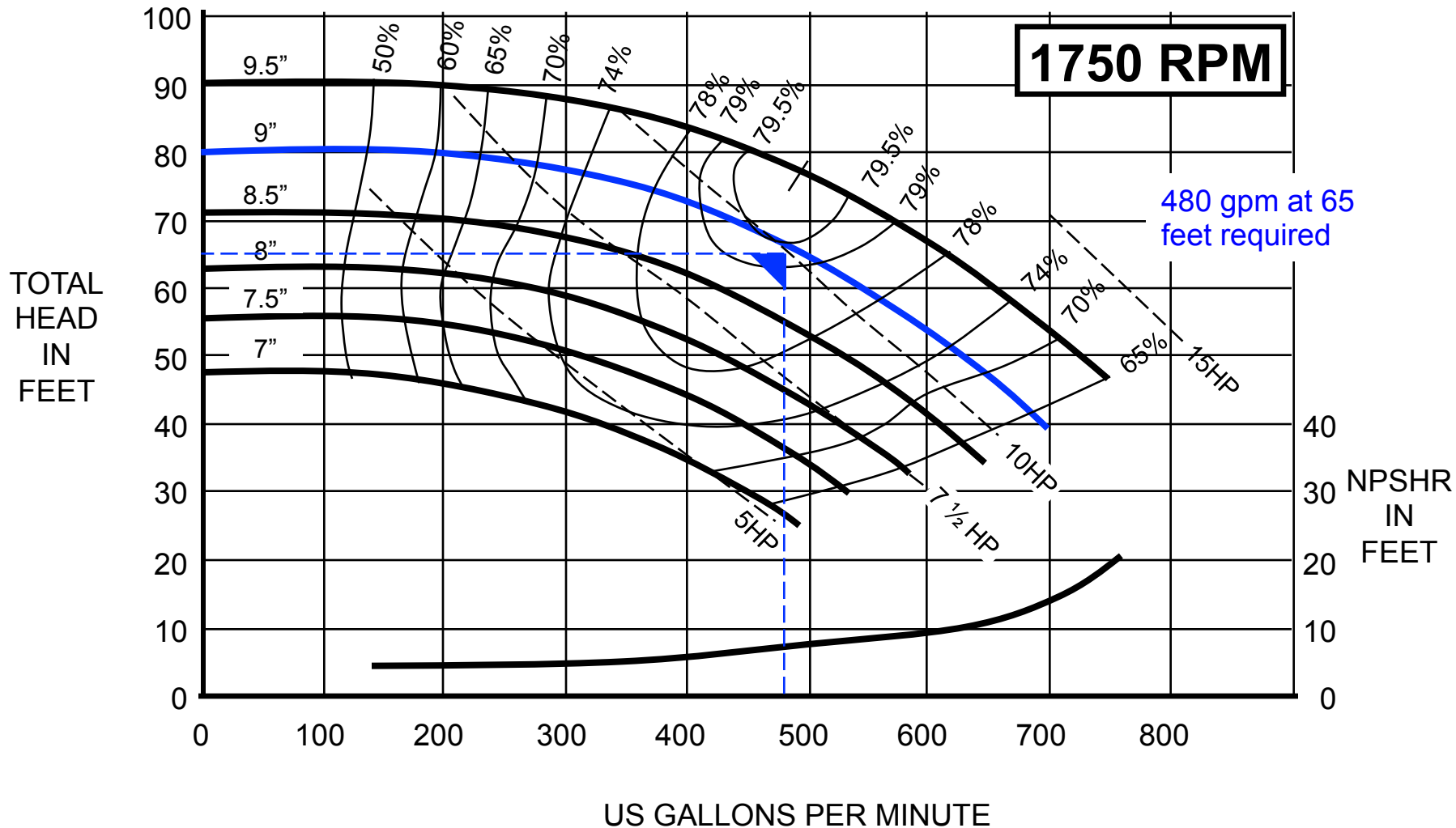


Source: Hydraulic Institute/Europump Guide to Life Cycle Costs

Typical Single Stage Pump Curve



Typical End Suction Pump Curve



Remember the Basics.....

Water horsepower (a.k.a. hydraulic horsepower)

$$P_3 = whp = \frac{Q \times H \times SG}{3960}$$

Q = Flow in gpm

H = Head in feet

SG = Specific Gravity of liquid

η = Pump Efficiency (Greek symbol "eta")

Brake horsepower (Pump Shaft)

$$P_2 = bhp = \frac{Q \times H \times SG}{3960 \times \eta_{pump}}$$

Electric horsepower (Input Power)

$$P_1 = ehp = \frac{bhp}{\eta_{driver}}$$

η_{driver} = driver efficiency

$$P_1 [kW] = ehp = \frac{bhp \times 0.746}{\eta_{motor} \times \eta_{drive}}$$